# **Dedication**

# To my mother

## **Acknowledgments**

To begin with, I would like to express my deep gratitude to my supervisor, Dr. El- fatih Ahmed Hassan. He gave me the opportunity not only to perform the research that led to this thesis, but also to promote my standing of Crude oil composition wax, Emulsions, and Asphaltenes phenomena. Moreover, I am very grateful for the permanent trust he .granted to me

I wish to express my thanks to the central petroleum .laboratories staff who, kindly, agreed to examine this work

I wish to thank Petrodar Operating Company (PDOC) They have brought real-size problems to my attention and provided real .data

I would like to address special thanks to the staff of the chemistry dept, college of science, Sudan University of science .and technology for their cooperation and support technical

Finally, I would especially like to record my gratefull appreciation for the tremendous amount of private time, . voluntarily given by Eng. Ossama Mohmed Mounsour

### **Abstract**

The Sudanese crude oil is regarded as one of the simplest types of crude in the world as it contains no percentage of sulfur which reacts with water to form sulfuric acid that negatively impact the production facilities and transportation lines due its corrosiveness. How ever it suffers other problems

represented by the high viscosity and high percentage of wax. These characteristics prevail in the crude oil produced by Petrodar company causing some very serious technical problems affectively the transfer of crude which is transported long distances from production fields to the port export terminal a .matter that affect directly the cost of production and the quality

A detailed study was made on the system adopted in collecting crude oil from different wells and physical and chemical processing to which crude is subjected through different stages of production and also study of the behaviour .of crude in the pipeline during transportation processes

Samples were collected from the fields of production at Adar-yale, Agordeed and Palouge and also samples were collected after the initial and final treatment .at CPF

No samples of the recently introduced field such as Gummry, Gasub, Moleeta, .were collected, but their specifications were inferred from available data

Physical and chemical properties that have been studies were amount of wax, is in the range 23-31% and asphaltene which was around 0.1%; resin content that ranged from 13-7%, deposits was 0.01%, water cut was 0.05% and the carbon number distribution in the crude which ranged between 7 to35 carbon atoms. The pour point was found range from 39-42 C; also the boiling point was in the range from 70  $^{\circ}\text{C}$  - 533+ C  $^{\circ}$  and density specifications according the .American Institute of petroleum was 24

Mechanical effects and temperature influence in viscosity were also studied. The composition of the Dar Blend was found to influence the flow characteristics of the crude. Presence of asphalting and resins reduce the .deposition of wax crystals and enhance, therefore, the fluidity of the crude

When increasing the rate of shear at a temperature higher than 42C doesn't .effect on viscosity, it became constant

The chemical additives effects on pour point and viscosity was studied. It was found that addition of PPD had no effect in altering the viscosity even at a dose .(of 1000-4000 ppm (i.e, ten folds greater than the usual dose

It is either unsuitable additives were used by Dar Company or the additives were expired, which in either case necessitate reevaluations of using such .additives

#### الخلاصة

يصنف الخام السوداني من ابسط أنواع الخام في العالم لعدم إحتوائه على نسبة عالية من الكبريت الذي يتفاعل مع الماء ليكون حمض الكبيرتيك ذو التأثير السلبي. ولكن هنالك مشاكل إخري متمثلة في اللزوجة العالية ونسب الشمع المرتفعة فيه وهذه الخصائص تسود في الخام المنتج بواسطة شركة بترودار مما تنتج عنه بعض المشاكل التقنية المتعلقة بنقل الخام وخاصة أن الخام ينقل إلي مسافات بعيدة من مناطق آبار الإنتاج إلى ميناء التصدير ممايؤثر مباشرة على تكلفة الإنتاج والجودة.

تمت دراسة تفصيلية لكيفية تجميع الخام من الآبار والمعالجات الكيميايئة والفيزئائية التي يتعرض لها عبر مراحل الإنتاج المختلفة وأيضاً دراسة لسلوكه داخل خط أنابيب نقل الخام.

تم جمع عينات من حقول إلانتاج عداريل وأكورديد وفلج كما تم جمع عينات بعد المعالجات الأولية والنهائية . وهنالك حقول أدخلت حديثة إلى دائرة الإنتاج لم تجمع منها عينات ولكن تم جمع وتحليل بياناتها ومواصفاتها وهي حقول قصب وقمري وموليتا .

الخواص الكيميايئة والفيزئائية التي تمت دراساتها وتحليلها للعينات المختلفة هي محتويات الخام من كمية الشمع التي تراوحت بين 23—31% والأسفلتين الذي بلغ حوالي 0.1% والراتنجات التي كانت 13-7% والرواسب التي وجدت 0.00% والماء الذي بلغت نسبته 0.05% و توزيع عدد زرات الكربون في سلاسل وجزئيات الخام التي تراوحت مابين 7 إلي 35 ذرة كربون, درجة الإنسكاب حيث تراوحت ما بين 39 و التي تراوحت مئوية , ودرجة الغليان ثم الكثافة ,حسب مواصفات المعهد الأمريكي للبترول, وكانت 24 كما تم قياس اللزوجة وتأثير العوامل الميكانيكية عليها وتأثير التغير في درجة الحرارة وتأثيرات إضافة المواد الكيميائية المخفضة لترسيب الشموع على مدى تخفيض اللزوجة.

وقد بينت الدراسة أن هنالك حقول بها نسب شمع عالية بينمـا أخـري لهـا نسـبة عاليـة من الأسفلتين والراتنجـات من الأسفلتين والراتنجـات إيجابى إذ أنه يمنع ترسيب جزئيات الشمع بفاعلية عالية ويزيد من سيولة الخام.

زيادة معدل القص عند درجة حرارة أعلي من 42 درجة مئويـة لا يـؤثر علـي اللزوجـة, حيث تصبح ثابتة عندئذ في مستوي معين .

كما بينت الدراسة أن حقن المعالج الكيمئايي الخافض لدرجة الإنسكاب ليس لديه أي فعالية بالرغم من إضافته بنسب عالية تراوحت من 1000 إلى 4000 جزء من المليون أي مايصل إلي عشرة أضعاف الكمية المعتادة مما يستوجب إعادة النظر من قبل شركة بترودار في إختيارها للمضافات الكيميائية خافضة درجة الإنسكاب أو التحقق من جودتها وصلاحيتها للإستخدام.

#### **Contents**

| Subject              | Page |
|----------------------|------|
| Dedication           | i    |
| Acknowledgement      | ii   |
| ( Abstract ( English | iii  |
| ( Abstract ( Arabic  | V    |
| Contents             | vi   |
| Tables               | xi   |

| Figures                                                   | xii  |
|-----------------------------------------------------------|------|
| Notation                                                  | xiii |
| CHAPTER ONE                                               |      |
| Introduction.1                                            | 1    |
| Types and Composition Of Crude Oil 1.1                    | 1    |
| Saturates hydrocarbon 1.1.1                               | 2    |
| Unsaturated hydrocarbons 1.1.2                            | 2    |
| Bitumen 1.1.3                                             | 3    |
| Physical properties of crude oil 1.2                      | 4    |
| Density 1.2.1                                             | 4    |
| Pour point 1.2.2                                          | 5    |
| Viscosity 1.2.3                                           | 5    |
| Boiling Point 1.2.4                                       | 6    |
| Melting Point 1.2.5                                       | 6    |
| Solubility Characteristics 1.2.6                          | 7    |
| Reid Vapour Pressure 1.2.7                                | 7    |
| Chemical Properties 1.2.8                                 | 7    |
| Thermal Reactions 1.2.9                                   | 8    |
| Oxidation Reactions 10 .1.2                               | 8    |
| Crud oil Industry In Sudan .1.3                           | 9    |
| :PDOC Melut Basin Oil Development process description.1.4 | 10   |
| Process in brief 1.4.1                                    | 10   |
| Palogue FSF system description 1.4.2                      | 13   |
| Well Head 1.4.3                                           | 13   |
| Flow lines and Trunks Lines 1.4.4                         | 14   |
| OGM 1.4.5                                                 | 14   |
| Operating/Design Parameters 1.4.6                         | 15   |

| Adar filed production facilities 1.5                   | 16 |
|--------------------------------------------------------|----|
| 1.5.1Crude Oil Process System                          | 16 |
| First Stage Separator 1.5.1.1                          | 16 |
| Second Stage Separator 1.5.1.2                         | 16 |
| Utility Facilities System 1.5.1.3                      | 17 |
| Palogue Field Production Facilities 1.6                | 19 |
| Crude oil receiving section 1.6.1                      | 19 |
| Inlet headers 1.6.1.1                                  | 19 |
| Three-phase metering skid 1.6.1.2                      | 19 |
| : Pig Receivers 1.6.1.3                                | 19 |
| Inlet Manifold 1.6.1.4                                 | 20 |
| Crude oil Processing 1.6.2                             | 22 |
| First Stage Separators 1.6.2.1                         | 22 |
| Second. Stage Separators and Crude Oil Heating 1.6.2.2 | 23 |
| Gas Boot 1.6.2.3                                       | 24 |
| Crude oil storage / exporting system 1.6.3             | 24 |
| The utility systems in FPF 1.6.4                       | 24 |
| (Aljabalayn Central Processing Facilities (CPF 1.7     | 26 |
| Crude oil system description 1.7.1                     | 26 |
| Process in brief 1.7.2                                 | 27 |
| Crude oil receiving system 1.7.3                       | 27 |
| Pigging Facilities 1.7.4                               | 27 |
| Crude oil processing 1.7.5                             | 27 |
| Surge vessels 1.7.5.1                                  | 28 |
| Dehydration Train 1.7.5.2                              | 30 |
| Crude /crude exchangers 1.7.5.2.1                      | 31 |
| 1.7.5.2.2Crude oil heaters                             | 31 |

| Electrostatic Dehydrater 1.7.5.2.3 31  Gas Boot 1.7.5.2.4 32  Crude oil storage and export facilities 1.7.6 32  Metering System 1.7.7 32 |
|------------------------------------------------------------------------------------------------------------------------------------------|
| Crude oil storage and export facilities 1.7.6 32                                                                                         |
|                                                                                                                                          |
| Metering System 1.7.7 32                                                                                                                 |
|                                                                                                                                          |
| Back Transport (YO-YO) operation 1.7.8 33                                                                                                |
| Utility Systems 1.7.9 33                                                                                                                 |
| Down Stream Facilities 1.7.10 33                                                                                                         |
| General Description 1.7.10.1 33                                                                                                          |
| Field Pipe Line 1.7.10.2 34                                                                                                              |
| Export Pipe Line 1.7.10.3 34                                                                                                             |
| Control system 1.7.10.4 36                                                                                                               |
| Chapter Two                                                                                                                              |
| Method and Materials .2 37                                                                                                               |
| Collection Of Crude Oil Samples 2.1 37                                                                                                   |
| :Methods 2.2 37                                                                                                                          |
| Determination Of Paraffin Wax Content 2.2.1 37                                                                                           |
| Apparatus and Reagents 2.2.1.1 37                                                                                                        |
| : Procedure 2.2.1.2 38                                                                                                                   |
| Calculation 2.2.1.3 38                                                                                                                   |
| Determination of asphaltene 2.2.2 38                                                                                                     |
| Apparatus and Reagents 2.2.2.1 39                                                                                                        |
| Procedure 2.2.2.2 39                                                                                                                     |
| Calculation 2.2.2.3 40                                                                                                                   |
| Determination 0f resins 2.2.3 42                                                                                                         |
| Apparatus and Reagents 2.2.3.1 42                                                                                                        |
| Procedure .2.2.3.2 <i>42</i>                                                                                                             |
| 2.2.3.3Calculation <i>42</i>                                                                                                             |

| Determination of Sediment 2.2.4                           | 43         |
|-----------------------------------------------------------|------------|
| Apparatus and Reagents 2.2.4.1                            | 43         |
| Procedure 2.2.4.2                                         | 43         |
| Calculation 2.2.4.3                                       | 43         |
| Determination of pour point 2.2.5                         | 44         |
| Apparatus and Reagent 5.1 .2.2                            | 44         |
| Procedure 2.2.5.2                                         | 44         |
| Determination of viscosity .2.2.6                         | 44         |
| Apparatus 2.2.6.1                                         | 45         |
| Procedure 6.2 2.2                                         | 45         |
| Determination of Carbon Number distribution by Gas .2.2.7 | 47         |
| Analysis of the Gas Chromatograph 2.2.7.1                 | 47         |
| Apparatus 2.2.7.2                                         | 47         |
| Procedure:2.2.7.3                                         | 47         |
| Determination of density and Relative Density by D .2.2.8 | 49         |
| Digital Density Analyzer 2.2.8.1                          | 49         |
| Apparatus 2.2.8.2                                         | 49         |
| Procedure 2.2.8.3                                         | 49         |
| Chapter Three                                             |            |
| Results & Discussion 3.1                                  | 52         |
| Conclusion 3.2                                            | <i>7</i> 9 |
| Reference                                                 | 80         |

## **List of Tables**

| Table                                                           | Page |
|-----------------------------------------------------------------|------|
| Typical distillation cuts produced in a refinery                | 6    |
| (Basic operation data (P/L Hydraulic steady state               | 35   |
| Basic operation data for all the intermediate stations          | 36   |
| Crude oil classification based on density at 15C                | 49   |
| Physical properties of Adar , Gummry , Moleeta , Palouge Fields | 52   |
| Contributions of different field in Dar Blend                   | 52   |
| wax content from different oil fields                           | 53   |
| Wax content from Inlet and out let of FPF                       | 54   |
| Dar blend Crude oil assay                                       | 55   |
| Asphaltene content                                              | 56   |
| Resin content                                                   | 57   |
| True boiling point distillation                                 | 65   |
| Viscosity @ varies Shear Rate                                   | 67   |
| Variation of Pour point with PPD dosage                         | 73   |

## List of Figures

| Figure                                                                                          | Page |
|-------------------------------------------------------------------------------------------------|------|
| Crude oil components                                                                            | 3    |
| Up stream facilities of PDOC                                                                    | 12   |
| overall schematic layout of Palogue FPF operation                                               | 21   |
| Aschamtic diagram for Surge Vessel                                                              | 29   |
| Dehydration Train                                                                               | 30   |
| Gas Chromatograph of Adar Crude                                                                 | 59   |
| Gas Chromatograph of Palouge Crude                                                              | 60   |
| Gas Chromatograph of mixture at palouge FPF                                                     | 61   |
| Gas Chromatograph of CPF out let Crude                                                          | 62   |
| Graph of True Boiling Point Against Graph of accumulated distillation                           | 64   |
| Viscosity versus Temperature at varies shear rate                                               | 67   |
| Viscosity versus increase in temperature                                                        | 68   |
| log viscosity versus log shear rate at 70 °C                                                    | 69   |
| log viscosity versus log shear rate at 50.1 °C                                                  | 69   |
| Viscosity versus shear rate at varies Temperature                                               | 70   |
| Sexthotropic behavior                                                                           | 71   |
| Pour Point with out PPD                                                                         | 73   |
| Pour Point with 4000 ppm PPD                                                                    | 74   |
| Pour Point with 3000 ppm PPD                                                                    | 75   |
| Blank Dar Blend Microscopic Image at Gel point 36°C                                             | 76   |
| Microscopic Image for Dar Blend Treated with 1500 ppm PPD at Gel point .36 $^{\circ}\mathrm{C}$ | 76   |

#### **Notations**

#### **Symbols**

P pressure

.μ Viscosity of fluid

Density of the fluid

#### **Subscripts**

API American Petroleum institute

**BS&W** Basic Sediment and Water

CCR Center Control Room

.CI Corrosion Inhibitor

Cp cent poise

Cs centistokes

.CPF Center processing facilities

#### ESD Emergency Shutdown

.ESP Electric Submersible Pumps

.FPF Field production facilities

FSF Field Surface Facilities

PDOC Petrodar operating company

.PCP Progressive Cavity Pumps

.PCV pressure control valve

.PPD Pour Point Depressant

PS Pump station

OGM Oil Gathering Manifold

MT Marine Terminal

MPM Multi phase meter

MPP Multiphase Pump

Temp Temperature

.SG Specific Gravity

.SI Scale Inhibitor

RVP Reid Vapor Pressure

.WCA Wax-control additives

.WI Wax Inhibitor