

DEDICATION

To my parents,

My husband

and My two sons and daughter

for their support and

encouragement throughout this study

Nahid

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NAHID

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Abbreviation

A	Cross – sectional area perpendicular to the direction of flow through – circulation drying, L^2
Ala	Alanine
Arg	Arginine
A_u, A_m	non drying surface and average area of the drying solid
B	Constant
G	Mass velocity of gas, $M / L^2 q$
Glu	Glutamic acid
Gly	Glycein
h_C	Heat transfer coefficient for convection $FL / L^2 T q$
h_R	Heat transfer coefficient for radiation, $FL / L^2 T q$
Hyp	Hydroxyproline
k_m	Thermal conductivity of tray, $FL^2 / L^2 q$
k_s	Thermal conductivity of drying solid, $FL^2 / L^2 q$
k_Y	Gas phase mass transfer coefficient, mass evaporated /(area)(time), (humidity deference), $M / L^2 q (M / M)$
M	Constant
N	Flux of drying mass of moisture evaporated /(area)(time), $M/L^2 \theta$ rate of revolution / θ
N_C	Constant flux of drying, $M/L^2 \theta$
N_m	is a logarithmic average of the rate N_1 , at a moisture content X_1 . , and N_2 at X_2
Pro	Proline
q_K	Heat flux for conduction, $FL/L^2 \theta$

q_C	Heat flux for convection, $FL/L^2\theta$
q_R	Heat flux for radiation, $FL/L^2\theta$
s	Slope of drier, L/L
S	Interfacial surface of solid /bed cross section, L^2/L^2
S_s	Mass of dry solid in a batch , batch drying M mass velocity of dry solid continuous drying , $M/L^2\theta$
t_G	Dry – bulb temperature of a gas, T
t_R	Temperature of radiating surface, T
t_s	A absolute temperature of surface, T
U_K	Over all heat – transfer coefficient $FL / L^2T q$
X	Moisture content of a solid, mass Moisture /mass dry solid , M/M
X^*	Equilibrium moisture content of a solid, mass Moisture /mass dry solid , M/M
y	Humidity (mass moisture/mass dry gas), M / L^2q
y_s	A absolute Humidity (mass moisture/mass dry gas), M / L^2q
Z	Length of drier, L
Z_M	Thickness of tray material, L
Z_s	Thickness of drying material, L
l_s	Latent heat of vaporization at t_s , FL/M
μ	Viscosity , $M/ L \theta$
Δ	Difference
ΔX	Change in moisture

$\Delta\theta$ Change in time
 θ time

Abstract

This study is undertaken to manufacture and utilize gelatin from splits and rejects of hides and skins in tanneries . The splits and rejects cow hides were taken from Al-Nasr tannery in limed conditions. The pelts were well washed and pickled in concentrated sulphuric acid diluted (1:10) using no salt to enhance gelatinization. The process of pickling was allowed to stay for 72 hours at a temp of 40 °C to allow complete gelatinization. The pelts were subjected to heating to concentrate the gelatin solution under a pressure of 1 bar and 70 °C.

The solution was cooled to room temperature, 27 °C and then filtered.

The viscosity of the thin liquor was measured and found to be 1.2 N.S/m². To raise the viscosity, the thin solution was subjected to evaporation in a single – effect evaporator, where the viscosity was increased to 1.8 N.S/m². Having set the procedure for the manufacturing process a two –level-factorial experiments were designed with factors including: temp, concentration, time and pressure, the experiments were carried out at low and high levels of each factor.

The factorial experiments showed that time and concentration were significant while temp has a negative effect as it reduces the viscosity, but on the contrary it speeded up the rate of gelatinization, on the other hand pressure was found to be insignificant. From the factorial experiments the optimum factors were specified and a controlled experiments were carried out to produce spray dried gelatin.

Gelatin has many utilization, it can be used as glue for pasting and in water – shut off in oil wells, hence it's adhesive power was investigated and found to be very strong (15.4N.S/m²), but caution must be taken in its application in deep oil wells as the temp. In such wells is high and may reduce the viscosity making the gelatin not be able to close the pores and water may come mixed with the oil.

صناعة الجلاتين من مخلفات الجلود

ملخص البحث

اهتمت هذه الدراسة بصناعة استخدام وصناعة الجلاتين من بقايا الجلود في المدايع. أخذت العينات المستخدمة من مدبغة النضر وهي في مرحلة الجير. غسلت العينات جيداً ثم أضيف حامض الكبريتيك المركز، وخفف بنسبة (1:10)، بدون استخدام أي ملح لتحسين عملية الجلتنة. تم حفظ العينات في الحامض لمدة 72 ساعة حتى تكتمل عملية الجلتنة. بعد اكتمال عملية الجلتنة، سخن المنتج تحت ضغط 1 bar في درجة حرارة 70 درجة مئوية وذلك لتركيز المنتج.

تم تبريد المنتج في درجة حرارة الغرفة (27 درجة مئوية) وبعد ذلك رشح المنتج وقيست لزوجته فكانت 1.2 نيوتن.ث/م². اخضع المنتج للتبخير وذلك لزيادة اللزوجة، فكانت 1.9 نيوتن.ث/م². ولضبط المنتج للصناعات المختلفة تم تصميم تجربتين عامليتين تحتويان على العوامل التالية: درجة الحرارة، التركيز، الزمن والضغط،، وأجريت التجارب في مستويين (عالي - منخفض) لكل العوامل. أوضحت التجارب العملية أن للزمن والتركيز أثر واضح في صناعة الجلاتين، بينما أن للحرارة أثر سالب وذلك لأنها تقلل من لزوجة المنتج على الرغم من أنها تزيد من عملية الجلتنة، من جانب آخر أوضحت التجارب أن الضغط لا يؤثر ظاهرياً في صناعة المنتج. من هذه التجارب العملية تم أخذ القياس لإنتاج مادة الجلاتين. للجلاتين استخدامات مختلفة فهو يستخدم كلاصق ويستخدم في آبار البترول لقفل المسامات وذلك لمنع اختلاط الماء بزيوت البترول. وأوضحت التجارب أنه فعال عندما يستخدم كلاصق إلا أن هناك بعض الاحتياطات عند استعماله في آبار البترول العميقة وذلك لارتفاع درجة الحرارة في باطن الأرض مما يؤثر على لزوجة الجلاتين ويكون غير فعال في قفل المسامات مما يؤدي الي اختلاط الماء بزيوت البترول.