

Sudan University of Science and Technology

# **Boiler Control Design Using Fuzzy Logic**

تصميم تحكم مرجل بإستخدام المنطق الغامض

A Thesis Submitted in Partial Fulfillment to the Requirements for the Degree of M.Sc. in Electrical Engineering (Microprocessor and Control)

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## الآيــة

(إِنَّ فِي خَلْقِ السَّمَاوَاتِ وَالْأَرْضِ وَاخْتِلَافِ اللَّيْلِ وَالنَّهَارِ وَالْفُلْكِ الَّتِي تَجْرِي فِي الْبَحْرِ بِمَا يَنفَعُ النَّاسَ وَمَا أَنزَلَ اللَّهُ مِنَ السَّمَاءِ مِن مَّاءٍ فَأَحْيَا بِهِ الْأَرْضَ بَعْدَ مَوْتِهَا وَبَثَّ فِيهَا مِن كُلِّ دَابَّةٍ وَتَصْرِيفِ الرِّيَاحِ وَالسَّحَابِ الْمُسَخَّرِ بَيْنَ السَّمَاءِ وَالْأَرْضِ لَآيَاتٍ لِّقَوْمٍ يَعْقِلُونَ)

صدق الله العظيم

سورة البقرة الآية (164)

# **DEDICATIONS**

This thesis is dedicated to:

The sake of Allah, my Creator and my Master,

My great teacher and messenger, Mohammed (May Allah bless and grant him), who taught us the purpose of life,

My great parents, who never stop giving of themselves in countless ways,

My beloved family and those people who have guided and inspired me throughout my journey of education.

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## ABSTRACT

In this study, a nonlinear dynamic model for large scale fossil fueled boiler turbine power generation units is presented. The challenge in controller design for these plants exists because they are typically nonlinear and multi-variable with multiple control objectives. This thesis presents the application of a fuzzy logic based controller for boiler turbine plant to control the drum pressure, power output and water level. Fuzzy control system have been successfully applied to a wide variety of practical problems. It has been shown that these controllers may perform better than conventional controllers especially when applied to processes difficult to model, with nonlinearities, and when there is heuristic knowledge from human operators.

The scopes includes the modelling, designing and simulation of boiler turbine, conventional controller PI and fuzzy controller. The models are carried out using MATLAB/SIMULINK. The simulation results demonstrate that performance of fuzzy logic controller is better.

## مستخلص

في هذه الدراسة تم تقديم نموذج ديناميكي لا خطي لوحدة توليد مرجل توربيني ذات وقود حجري واسعة النطاق. ويكمن التحدي في تصميم نظام تحكم لهذه الوحدات بسبب انها لا خطية ومتعددة المتغيرات وذات أهداف تحكم متعددة. يقدم هذا البحث تطبيق وحدة تحكم منطق غامض للمرجل التوربيني للتحكم في ضغط الاسطوانة والقدرة الخارجة ومستوي المياه. انظمة التحكم الغامض طبقت بنجاح على مجموعة واسعة من المشاكل العلمية وقد ثبت ان اداء هذه المتحكمات أفضل من المتحكمات التقليدية، وخصوصا عندما تطبق على عمليات ذات طبيعة لا خطية مع صعوبة ايجاد النموذج لها، وعندما يكون هناك حوجه للخبرة المعرفية للعاملين.

ويشمل النطاق النمذجة وتصميم ومحاكاة للمرجل التوربيني والمتحكم التناسبي-التكاملي التقليدي والمتحكم الغامض. تم تنفيذ النماذج باستخدام MATLAB/SIMULINK. نتائج المحاكاة اثبتت ان أداء متحكم المنطق الغامض هو الأفضل.

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# LIST OF ABBREVIATIONS

ASME	American Society of Mechanical Engineers
СЕ	Change in Error
D	Derivative
Е	Error
FIS	Fuzzy Inference Systems
FLC	Fuzzy Logic Controller
GUI	Graphical User Interface
Ι	Integral
MIMO	Multiple Input and Multiple Output
MISO	Multiple Input and Single Output
Р	Proportional
PC	Personal Computer
PI	Proportional Integral
PID	Proportional Integral Derivative
R	Reference
TSK	Takagi-Sugeno- Kang

# LIST OF SYMBOLS

μ <sub>A</sub>	Membership function
k <sub>d</sub>	Derivative gain
k <sub>i</sub>	Integral gain
k <sub>p</sub>	Proportional gain
k <sub>u</sub>	Ultimate gain
T <sub>u</sub>	Oscillation period
U	Control signal
Y	Actual output

# **CHAPTER ONE**

# **INTRODUCTION**

# CHAPTER ONE INTRODUCTION

### **1.1 Overview**

The steam generator or boiler turbine is an integral component of a steam engine when considered as a prime mover. However it needs be treated separately, as to some extent a variety of generator types can be combined with a variety of engine units. A boiler incorporates a firebox or furnace in order to burn the fuel and generate heat. The generated heat is transferred to water to make steam. This produces saturated steam at a rate which can vary according to the pressure above the boiling water. The higher the furnace temperature, the faster the steam production. The saturated steam thus produced can then either be used immediately to produce power via a turbine and alternator, or else may be further superheated to a higher temperature, this notably reduces suspended water content making a given volume of steam produce more work and creates a greater temperature gradient, which helps reduce the potential to form condensation. Any remaining heat in the combustion gases can then either be evacuated or made to pass through an economizer, the role of which is to warm the feed water before it reaches the boiler [1].

A practical control problem that has received a great deal of attention lately, is the robust control of power plants. It is well known that automatic control is deemed a necessary condition for safe operation which minimizes material fatigue, the number of staff, and enables efficient plant management. However, the design of controllers for power plants is not a trivial task. The challenge in controller design for these plants exists because they are typically non-linear and multivariable with multiple control objectives. While conventional controls such as Proportional Integral Derivative (PID) controller compensators yield an acceptable response, they do not have the flexibility necessary to provide a good performance over a wide region of operation [2].

Fuzzy logic represents soft computing method for solving problems where classical logic cannot provide satisfying results. Fuzzy logic is multi-value logic derived from theory of fuzzy sets proposed by L. A. Zadeh (1965). This kind of logic gained

success because it makes use of the tolerance for imprecision and uncertainty to achieve tractability, robustness, and low cost solution. The key quality of fuzzy logic standpoint is the possibility of giving a formal and procedural representation of linguistic terms used to state human centered concepts [3].

The concept of intelligent control lies with the fact that human intelligence is imbibed in to the controller architecture so that human behavior can be emulated in the control decision. Human expert knowledge is based upon heuristic information gained in relation to the operation of the plant or process, and its inherent vagueness ("fuzziness") offers a powerful tool for the modeling of complex systems. The fuzzy logic controller provides an algorithm, which converts the expert knowledge into an automatic control strategy. Fuzzy logic is capable of handling approximate information in a systematic way and therefore it is suited for controlling nonlinear systems and is used for modeling complex systems where an inexact model exists or systems where ambiguity or vagueness is common. The fuzzy control systems are rule based systems in which a set of fuzzy rules represent a control decision mechanism to adjust the effects of certain system stimuli. With an effective rule base, the fuzzy control systems can replace a skilled human operator. The rule base reflects the human expert knowledge, expressed as linguistic variables, while the membership functions represent expert interpretation of those variables [4].

#### **1.2 Problem Statement**

Boiler is the main component of generating steam in thermal power generation units and its control is very important in many applications. In present situation conventional PID control is being used for this purpose. These conventional controllers in power plants are not very stable when there are fluctuations and, in particular, when there is an emergency occurring. Continuous processes in power plant and power station are complex systems characterized by nonlinearity, uncertainty and load disturbances. The conventional controllers do not work accurately in a system with nonlinearity.

## **1.3 Objectives**

The main objectives of this study are to:

- Develop of boiler turbine system model.
- Design of Proportional Integral (PI) controller for boiler turbine system.
- Design of fuzzy logic controller for boiler turbine system.
- Comparison of controller's response.

## **1.4 Methodology**

- The proposed method consists of two sections. First section concerns with pressure and power output control and the second section consists of water level control system. For both of the sections fuzzy logic control is designed.
- The system variables and components are modeled and simulation is done using MATLAB / SIMULINK software.

## 1.5 Layout

This thesis consists of five chapters including this chapter. Chapter one gives an introduction, problem statement for this study. It also presents the objectives and methodology of this study. Chapter two gives a theoretical background, discuss briefly the basic construction of boiler, then list of classification, fuzzy control system and conventional (PID) controller. Chapter three mainly focusing on the mathematical modeling and simulation of the boiler using MATLAB/SIMULINK. Secondly, the design of PI controller and fuzzy logic controller are described. Chapter four handles the simulation results and discussion. Finally chapter five presents conclusions and recommendations.

# **CHAPTER TWO**

# THEORETICAL BACKGROUND

# CHAPTER TWO THEORETICAL BACKGROUND

## 2.1 Boiler

Boilers are manufactured in many different sizes and configurations depending on the characteristics of the fuel, the specified heating output, and the required emissions controls. Figure 2.1 shows the industrial boiler, some boilers are only capable of producing hot water, while others are designed to produce steam. Combustion boilers are designed to use the chemical energy in fuel to raise the energy content of water so that it can be used for heating and power applications. Many fossil and non-fossil fuels are fired in boilers, but the most common types of fuel include coal, oil, and natural gas. During the combustion process, oxygen reacts with carbon, hydrogen, and other elements in the fuel to produce a flame and hot combustion gases. As these gases are drawn through the boiler, they cool as heat is transferred to water. Eventually the gases flow through a stack and into the atmosphere. As long as fuel and air are both available to continue the combustion process, heat will be generated [5].



Figure 2.1: Industrial boiler

## 2.1.1 Operation

The separated steam is drawn out from the top section of the drum and distributed for process. Further heating of the saturated steam will make superheated steam normally used to drive a steam turbine. Saturated steam is drawn off the top of the drum and re-enters the furnace in through a superheater. The steam and water mixture enters the steam drum through riser tubes, drum internals consisting of demister separate the water droplets from the steam producing dry steam. The saturated water at the bottom of the steam drum flows down through the downcomer pipe, normally unheated, to headers and water drum. Its accessories include a safety valve, waterlevel indicator and level controller. Feed-water of boiler is also fed to the steam drum through a feed pipe extending inside the drum, along the length of the steam drum. A steam drum is used without or in the company of a mud-drum/feed water drum which is located at a lower level. A boiler with both steam drum and mud/water drum is called a bi-drum boiler and a boiler with only a steam drum is called a mono-drum boiler. The bi-drum boiler construction is normally intended for low pressure-rating boiler while the mono-drum is mostly designed for higher pressure-rating [6].

#### **2.1.2 Boiler types**

Boilers can be classified in many types:

i. Horizontal, vertical or inclined

If the axis of the boiler is horizontal, vertical or inclined then it is called horizontal, vertical or inclined boiler respectively.

ii. Fire tube and water tube

If hot gases are inside the tube and water is outside the tube, it is called firetube boiler as shown in Figure 2.2. Examples: Cochran, Lancashire and locomotive boilers. If water is inside the tube and hot gases are outside the tube, it is called water-tube boiler as shown in Figure 2.3. Examples: Babcock and Wilcox, Sterling, Yarrow boiler etc.

- iii. Externally fired and internally fired
  The boiler is known as externally fired if the fire is outside the shell.
  Examples: Babcock and Wilcox, Sterling
  The boiler is known as internally fired if the furnace is located inside the boiler shell. Examples: Cochran, Lancashire.
- iv. Forced circulation and natural circulation
   In forced circulation type of boilers, the circulation of water is done by a forced pump. Examples: Velox, Lamont, Benson boiler. In natural circulation

type of boilers, circulation of water in the boiler takes place due to natural convection currents produced by the application of heat. Examples: Lancashire, Babcock and Wilcox.



Figure 2.2: Fire tube boiler



Figure 2.3: Water tube boiler 6

v. High pressure and low pressure

The boilers which produce steam at pressures of 80 bar and above are called high pressure boilers. Examples: Babcock and Wilcox, Velox, Lamont, Benson boilers. The boilers which produce steam at pressure below 80 bars are called low pressure boilers. Examples: Cochran, Cornish, Lancashire and locomotive boilers.

- vi. Stationary and portable (moving).
  Stationary boilers are used for power plant-steam, for central station utility power plants, for plant process steam etc. Mobile or portable boilers include locomotive type, and other small unit for temporary use at sites.
- vii. Single tube and multi tube

The fire tube boilers are classified as single tube or multi-tube boilers, depending upon whether the fire tube is one or more than one. Examples of single tube boilers are Cornish and simple vertical boiler [5].

#### **2.1.3 Boiler circulation**

Boilers generate steam using different methods to circulate the steam-water mixture is inside the tubes and is heated by external combustion flames and flue gases. The water tube boilers are classified by the way of the water/steam circulation:

i. Natural circulation

The natural circulation is one of the oldest principles for steam/water circulation in boilers. Its use has decreased during the last decades due to technology advances in other circulation types. Natural circulation principle is usually implemented on small and medium sized boilers. Typically the pressure drop for a natural circulation boiler is about 5-10 % of the steam pressure in the steam drum and the maximum steam temperature varies from 540 to 560 °C.

ii. Assisted or forced circulation

In contrast to natural circulation boilers, forced circulation is based on pumpassisted internal water/steam circulation. The circulation pump is the main difference between natural and forced circulation boilers. In the most common forced circulation boiler type, the Lamont boiler, the principles of forced circulation is basically the same as for natural circulation, except for the circulation pump.

The operation pressure level of forced circulation boiler can be slightly higher than a natural circulation boiler, but since the steam/water separation in the steam drum is based on the density difference between steam and water, these boilers are not either suitable for supercritical pressures (>221 bar). Practically the maximum operation pressure for a forced circulation boiler is 190 bar and the pressure drop in the boiler is about 2-3 bar.

iii. Once-through

A once-through (or universal pressure) boiler can be simplified as a long, externally heated tube. There is no internal circulation in the boiler, thus the circulation ratio for once-through boilers is 1. In contrast to other water tube boiler types (natural and controlled circulation), once through boilers do not have a steam drum. Thus, the length of the evaporator part (where saturated water boils into steam) is not fixed for once through boilers.

Once-through boilers are also called universal pressure boilers because they are applicable for all pressures and temperatures. However, once through boilers are usually large sized boilers with high subcritical or supercritical steam pressure. A large modern power plant unit (about 900MW/h) based on the once-through design can be over 160m high with a furnace height of 100m.

iv. Combined circulation

This boiler type is a combination of controlled circulation boilers and oncethrough boilers. Combined circulation (once-through with superimposed recirculation) boilers can be used for both subcritical and supercritical steam pressure operation.

When the firing rate is between 60 and 100%, the boiler operates as a oncethrough boiler. At lower than 60% capacity load, combined circulation boilers operate as forced circulation boilers in idea to maintain adequate water/steam flow in wall tubes.

The biggest advantage of combined circulation type boilers is reduced demand of pump energy because the operation mode changes depending on the capacity load. Main disadvantages are the troublesome co-operation between feed water pump and circulation pump and also the high level needed for water treatment (as needed for once through boilers) [5].

#### 2.1.4 Material of boiler

The pressure vessel in a boiler is usually made of steel or alloy steel, or historically of wrought iron. Stainless steel is virtually prohibited by American Society of Mechanical Engineers (ASME) boiler code for use in wetted parts of modern boilers, but is used often in super heater sections that will not be exposed to liquid boiler water. In live steam models, copper or brass is often used because it is more easily fabricated in smaller size boilers. Historically, copper was often used for fireboxes particularly for steam locomotives, because of its better formability and higher thermal conductivity, however, in more recent times, the high price of copper often makes this an uneconomic choice and cheaper substitutes such as steel are used instead.

For much of the Victorian age of steam, the only material used for boiler making was the highest grade of wrought iron, with assembly by riveting. This iron was often obtained from specialist ironworks, such as at Celator Moor, noted for the high quality of their rolled plate and its suitability for high reliability use in critical applications, such as high pressure boilers. In the 20th century, design practice instead moved towards the use of steel, which is stronger and cheaper, with welded construction, which is quicker and requires less labour. Cast iron may be used for the heating vessel of domestic water heaters. Although such heaters are usually termed boilers, their purpose is usually to produce hot water, not steam, and so they run at low pressure and try to avoid actual boiling [7].

#### 2.1.5 Fuel for boiler

The source of heat for a boiler is combustion of any of several fuels, such as wood, coal, oil, or natural gas. Electric steam boilers use resistance or immersion type heating elements. Nuclear fission is also used as a heat source for generating steam. Heat recovery steam generators use the heat rejected from other processes such as gas turbines [7].

### 2.1.6 Boiler control

A steam boiler is a complex system consists of numerous components. The pressure variation phenomena inside a furnace of a steam boiler affect the steam boiler's efficiency and safety. A boiler is an enclosed vessel that provides a means for converting water into steam. The steam under pressure is then used for transferring the heat to a process. Water is a useful and cheap medium for transferring heat to a process. When water is boiled its volume increases by about 1600 times, producing a force that is almost as explosive as gunpowder. This causes the boiler to be extremely dangerous and must be treated with a lot of care.

The boiler's operating conditions is very necessary to control because the high pressures and temperatures are the main hazard problems and it has the risk of explosion. Also steam boiler has very high manufacturing cost, operating cost and maintenance cost. The operating conditions of steam boiler are very complex to control because all the variables (pressure, temperature, flow, level) are interrelated. Taking measurement directly on boiler is very difficult due to dangers from the operating conditions and not economical [8].

## **2.1.7 Boiler applications**

Boilers have many applications in the industries, research and development, etc. Some are listed below:

- They can be used in stationary applications to provide heat, hot water, or steam for domestic use, or in generators.
- They can be used in mobile applications to provide steam for locomotion in applications such as trains, ships, and boats.
- Using a boiler is a way to transfer stored energy from the fuel source to the water in the boiler, and then finally to the point of end use.
- Some steam boats, particularly smaller types such as river launches, were designed around a vertical boiler.
- The Sentinel Waggon works also produced a range of road lorries also known as steam wagons, based on their high-pressure vertical boilers [9].

## 2.2 Proportional-Integral-Derivative Controller

The PID controller is the most common form of feedback. It was an essential element of early governors and it became the standard tool when process control emerged in the 1940s. In process control today, more than 95% of the control loops are of PID type, most loops are actually PI control. PID controllers are the largest number of controllers found in industries sufficient for solving many control problems [10]. There are stand-alone systems in boxes for one or a few loops, which are manufactured by the hundred thousand yearly. PID control is an important ingredient of a distributed control system. The controllers are also embedded in many special-purpose control systems. PID control is often combined with logic, sequential functions, selectors, and simple function blocks to build the complicated automation systems used for energy production, transportation, and manufacturing. Many sophisticated control strategies, such as model predictive control, are also organized hierarchically. PID control is used at the lowest level; the multivariable controller gives the set points to the controllers at the lower level [11].

PID controllers have survived many changes in technology, from mechanics and pneumatics to microprocessors via electronic tubes, transistors, integrated circuits. The microprocessor has had a dramatic influence on the PID controller. Practically all PID controllers made today are based on microprocessors. This has given opportunities to provide additional features like automatic tuning, gain scheduling, and continuous adaptation [11].

#### 2.2.1 The three-term controller

The transfer function of the PID controller looks like the following:

$$k_{p} + \frac{k_{i}}{s} + k_{d}s = \frac{k_{d}s^{2} + k_{p}s + k_{i}}{s}$$
(2.1)

Where

- k<sub>p</sub> = Proportional gain
- k<sub>i</sub>= Integral gain
- $k_d$  = Derivative gain

First, let's take a look at how the PID controller works in a closed-loop system using the schematic shown in Figure 2.4. The variable Error (e) represents the tracking error, the difference between the desired input value (R) and the actual output (Y). This error signal (e) will be sent to the PID controller, and the controller computes both the derivative and the integral of this error signal. The signal (u) just past the controller is now equal to the proportional gain  $(k_p)$  times the magnitude of the error plus the integral gain  $(k_i)$  times the integral of the error plus the derivative gain  $(k_d)$ times the derivative of the error.

$$u = k_p e + k_i \int e \, dt + k_d \frac{de}{dt}$$
(2.2)

This signal (u) will be sent to the plant, and the new output (Y) will be obtained. This new output (Y) will be sent back to the sensor again to find the new error signal (e). The controller takes this new error signal and computes its derivative and it's integral again. This process goes on and on [12].



Figure 2.4: Unity feedback system

#### 2.2.2 The characteristics of PID controllers

A proportional controller  $(k_p)$  will have the effect of reducing the rise time and will reduce, but never eliminate, the steady-state error. An integral control  $(k_i)$  will have the effect of eliminating the steady-state error, but it may make the transient response worse. A derivative control  $(k_d)$  will have the effect of increasing the stability of the system, reducing the overshoot, and improving the transient response. Effects of each of controllers  $k_p$ ,  $k_d$ , and  $k_i$  on a closed-loop system are summarized in the Table 2.1. Note that these correlations may not be exactly accurate, because  $k_p$ ,  $k_i$ , and  $k_d$ are dependent of each other. In fact, changing one of these variables can change the effect of the other two. For this reason, the table should only be used as a reference when you are determining the values for  $k_i$ ,  $k_p$  and  $k_d$  [12].

Close Loop	Rise Time	Overshoot	Settling Time	Steady State
Response				Error
k <sub>p</sub>	Decrease	Increase	Small change	Decrease
k <sub>i</sub>	Decrease	Increase	Increase	Eliminate
k <sub>d</sub>	Small change	Decrease	Decrease	Small change

Table 2.1: PID controller characteristics parameters

#### 2.2.3 PID tuning

Tuning the PID controller is the adjustment of its control parameters  $(k_p, k_i \text{ and } k_d)$  to the optimum values for the desired control response. The PID tuning is a difficult problem, even though there are only three parameters and in principle is simple to describe, because it must satisfy complex criteria within the limitations of PID control. There are accordingly various methods for loop tuning, the some traditional manual methods for loop tuning, are presented below

#### i. Manual tuning

If the system must remain online, one tuning method is to first set  $k_i$  and  $k_d$  values to zero. Increase the  $k_p$  until the output of the loop oscillates, then the  $k_p$  should be set to approximately half of that value for a "quarter amplitude decay" type response. Then increase  $k_i$  until any offset is corrected in sufficient time for the process. However, too much  $k_i$  will cause instability. Finally, increase  $k_d$ , if required, until the loop is acceptably quick to reach its reference after a load disturbance. However, too much  $k_d$  will cause excessive response and overshoot. A fast PID loop tuning usually overshoots slightly to reach the setpoint more quickly; however, some systems cannot accept overshoot, in which case an over-damped closed-loop system is required, which will require a  $k_p$  setting significantly less than half that of the  $k_p$ setting that was causing oscillation.

#### ii. Ziegler-Nichols method

Another heuristic tuning method is formally known as the Ziegler–Nichols method, introduced by John G. Ziegler and Nathaniel B. Nichols in the 1940s. As in the method above, the  $k_i$  and  $k_d$  gains are first set to zero. The proportional gain is increased until it reaches the ultimate gain,  $k_u$ , at which the output of the loop starts to oscillate.  $k_u$  and the oscillation period  $T_u$  are used to set the gains as shown in Table 2.2.

Control Type	k <sub>p</sub>	k <sub>i</sub>	k <sub>d</sub>
Р	$0.5k_u$	-	-
PI	$0.45k_u$	$0.54k_u/T_u$	-
PID	0.6k <sub>u</sub>	$1.2k_u/T_u$	3k <sub>u</sub> T <sub>u</sub> /40

Table 2.2: Ziegler–Nichols method

#### iii. PID tuning software

Most modern industrial facilities no longer tune loops using the manual calculation methods shown above. Instead, PID tuning and loop optimization software are used to ensure consistent results. These software packages will gather the data, develop process models, and suggest optimal tuning. Some software packages can even develop tuning by gathering data from reference changes [12].

## 2.3 Fuzzy Logic

Fuzzy logic is extension of boolean logic. It incorporates partial values of truth. Instead of sentences being completely true or completely false, here in fuzzy logic they are assigned a value which represents their degree of truthiness. In fuzzy systems, values are indicated by a number called as truth value. It lies in the range from 0.0 to 1.0 represents absolute falseness and 1.0 represents absolute truth. Fuzzification is generalization of theory from discrete to continuous. Fuzzy logic is important to artificial intelligence. Fuzzy logic allows computers to answer to a certain degree unlike Boolean logic which gives one extreme or the other. Computers are allowed to think more humanlike. Nothing in our perception is extreme. However, it is true only to a certain degree. In fuzzy logic, machines think in degrees.

It can solve problems in the cases where there is no simple mathematical model. Fuzzy logic solves highly nonlinear processes. Fuzzy logic uses expert knowledge to make decisions [13].

Fuzzy logic was first invented as a representation scheme. It acts as calculus for uncertain or vague notions. It allows more human-like interpretations. Fuzzy logic has put reasoning in machines by resolving intermediate categories between notations like true/false, hot/cold etc. Fuzzy logic is a problem-solving control system methodology. It lends itself to implementation in systems ranging from small, simple, embedded microcontrollers to large, multi-channel, networked Personal Computer (PC) or workstation-based data acquisition control systems etc. It can be implemented in software, hardware, or a combination of both. Fuzzy logic provides a simple way to arrive at a definite conclusion. Conclusion is based upon ambiguous or vague, noisy, imprecise, or missing input information. Fuzzy logic's approach to control problems simply mimics how a person will make efficient decisions much faster [13].

In 1965, professor L.A. Zadeh of the University of California, Berkely presented his paper outlining fuzzy theory in which he introduced the concept of fuzzy set theory and operation, fuzzy logic based controller etc. In about 1970, fuzzy logic theory began to produce result in Japan, Europe and China. In the year 1987, 16 station subway railway systems were built which worked with a fuzzy logic-based automatic train operation control system in Sendai, Japan. The ride is so smooth that the riders do not need to hold straps, and the controller makes seventy percent fewer judgmental errors in acceleration and braking than human operators do. Fuzzy logic is a powerful problem-solving methodology with a myriad of applications in embedded control and information processing. Fuzzy provides a remarkably simple way to draw definite conclusions from vague, ambiguous or imprecise information. In a sense, fuzzy logic resembles human decision making with its ability to work from approximate data and find precise solutions. Unlike classical logic, which requires a deep understanding of a system, exact equations, and precise numeric values, fuzzy logic incorporates an alternative way of thinking, which allows modelling complex systems using a higher level of abstraction originating from our

knowledge and experience. Fuzzy logic allows expressing this knowledge with subjective concepts such as very hot, bright red, and a long time, which are mapped into exact numeric ranges [14].

Fuzzy logic is a paradigm for an alternative design methodology, which can be applied in developing both linear and non-linear systems for embedded control. Fuzzy logic provides an alternative solution to non-linear control because it is closer to the real world. Rules, membership functions, and the inference process which results in improved performance, simpler implementation, and reduced design costs handle non-linearity. By using fuzzy logic, designers can realize lower development costs, superior features, and better end product performance. Furthermore, products can be brought to market faster and more cost-effectively. Fuzzy logic has been gaining increasing acceptance during the past few years. There are over two thousand commercially available products using fuzzy logic, ranging from washing machines to high-current trains. Nearly every application can potentially realize the benefits of fuzzy logic [15].

#### 2.3.1 Fuzzy logic features

Fuzzy logic offers several unique features that make it a particularly good choice for many control problems.

- It is inherently robust since it does not require precise, noise-free inputs and can be programmed to fail safely if a feedback sensor quits or is destroyed. The output control is a smooth control function despite a wide range of input variations.
- Since the fuzzy logic controller processes user-defined rules governing the target control system, it can be modified and tweaked easily to improve or drastically alter system performance. New sensors can easily be incorporated into the system simply by generating appropriate governing rules.
- Fuzzy logic is not limited to a few feedback inputs and one or two control outputs, nor is it necessary to measure or compute rate-of-change parameters in order for it to be implemented. Any sensor data that provides some indication of a system's actions and reactions is sufficient. This allows the

sensors to be inexpensive and imprecise thus keeping the overall system cost and complexity low.

- Because of the rule-based operation, any reasonable number of inputs can be processed and numerous outputs generated, although defining the rule base quickly becomes complex if too many inputs and outputs are chosen for a single implementation since rules defining their interrelations must also be defined. It would be better to break the control system into smaller chunks and use several smaller fuzzy logic controllers distributed on the system, each with more limited responsibilities.
- Fuzzy logic can control nonlinear systems that would be difficult or impossible to model mathematically [15].

#### 2.3.2 The designing of fuzzy logic

- Define the control objectives and criteria: What am I trying to control? What do I have to do to control the system? What kind of response do I need? What are the possible system failure modes?
- Determine the input and output relationships and choose a minimum number of variables for input to the fuzzy logic engine, typically that are error and rate of change of error.
- Using the rule-based structure of fuzzy logic, break the control problem down into a series of IF X AND Y THEN Z rules that define the desired system output response for given system input conditions. The number and complexity of rules depends on the number of input parameters that are to be processed and the number fuzzy variables associated with each parameter. If possible, use at least one variable and its time derivative. Although it is possible to use a single, instantaneous error parameter without knowing its rate of change, this cripples the system's ability to minimize overshoot for a step inputs.
- Create fuzzy logic membership functions that define the meaning or values of input/output terms used in the rules.
- Test the system, evaluate the results, tune the rules and membership functions, and retest until satisfactory results are obtained [15].

#### 2.3.3 Operations

Fuzzy logic requires some numerical parameters in order to operate such as what is considered significant error and significant rate of change of error, but exact values of these numbers are usually not critical unless very responsive performance is required in which case empirical tuning would determine them [16].

### 2.3.4 Fuzzy logic types

These two types of fuzzy sets are explained in the following sections:

## A- Type I fuzzy set

Let X be a collection of objects called universe of discourse. A fuzzy set  $A \in X$  is characterized by membership function  $\mu_A(X)$  which represents the degree of membership. Degree of membership maps each element between 0 and 1. It is defined as:

$$A = \{(x, \mu_A(X)); x \in X\}$$
(2.3)

Figure 2.5 shows the triangular membership function with three linguistic variables as small, medium and large. For X = 18.75, degree of membership for small is 0.6 and degree of membership for medium is 0.4.

#### B- Type II fuzzy set

The type-2 fuzzy set model makes use of an extra third dimension. These sets are typically implemented as points stored in an array. Type-2 fuzzy logic requires two different levels of discretization: for the primary and secondary membership functions. In the case of generalized type-2 membership functions, where the secondary is a type-1 fuzzy number, the computational complexity is very large [16].

#### 2.3.5 Fuzzy inference system

Fuzzy Inference Systems (FIS) are rule-based systems. It is based on fuzzy set theory and fuzzy logic. FIS are mappings from an input space to an output space. FIS allows constructing structures which are used to generate responses or outputs for certain stimulations or inputs. Response of FIS is based on stored knowledge or relationships between responses and stimulations. Knowledge is stored in the form of a rule base. Rule base is a set of rules. Rule base expresses relations between inputs of system and its expected outputs [16].



Figure 2.5: Fuzzy logic membership function

Knowledge is obtained by eliciting information from specialists. These systems are usually known as fuzzy expert systems. Another common denomination for FIS is fuzzy knowledge-based systems. It is also called as data-driven fuzzy systems. FIS are usually divided in two categories viz. Multiple Input and Multiple Output (MIMO) systems and Multiple Input and Single Output (MISO) systems, the system returns several outputs based on the inputs which it receives. Multiple input and single output systems are those where only one output is returned from multiple inputs. MIMO systems are decomposed into a set of MISO systems which work in parallel.

Figure 2.6 shows the block diagram of fuzzy logic system. It has different blocks: fuzzifier, knowledge base, inference unit and defuzzifier.

In terms of inference process there are two main classes of FIS:

A- Mamdani based FIS

In mamdani based fuzzy inference system, inputs and outputs have an If-Then rules. A typical rule in a mamdani fuzzy model is: IF X is Negative Big AND Y is Negative Small THEN Z is Zero.



Figure 2.6: Block diagram of fuzzy logic system

#### B- Sugeno based FIS

Sugeno-type systems are used to model any inference system in which output membership functions are either linear or constant. This fuzzy inference system was introduced in 1985. It is also called as Takagi-Sugeno-Kang. Sugeno output membership functions (z) are either linear or constant. A typical rule in a Sugeno fuzzy model is:

If Input 1 = x and Input 2 = y, then Output is z = ax + by + c.

For a zero-order Sugeno model, the output level z is a constant (a=b=0). Figure 2.7 shows the rule viewer of the fuzzy logic system in case of mamdani inference system. The rule viewer shows one calculation at a time and in great detail.



Figure 2.7: Fuzzy rule base in the case of a mamdani fuzzy inference system
Both sugeno and mamdani FIS can be used to perform the similar tasks. Rule base and fuzzification remain same for the variables. There are various defuzzifiers that can be chosen for a mamdani FIS. These defuzzifiers also originate similar results in a sugeno FIS. There is a certain overlap between both types of systems. Mamdani FIS is more widely used. It is used for decision support applications, because of its intuitive and interpretable nature. Consequences of the rules in a sugeno FIS do not have a direct semantic mean. This means that they are not linguistic terms. Also, this interpretability is partially lost. Sugeno FIS rules consequents can have many parameters per rule as per input values. Thus, sugeno FIS gets translated into more degrees of freedom in its design as compared to mamdani FIS. Thus it provides more flexibility. Many parameters can be used in the consequents of the rules of a sugeno FIS. A zero order sugeno FIS can reasonably approximate a mamdani FIS. In computational terms, a sugeno FIS is more efficient than a mamdani FIS. It is so because, sugeno FIS does not involve computationally expensive defuzzification process. Also, a sugeno FIS always generates continuous surfaces. The continuity of the output surface is quite important. Any existence of discontinuities will result in similar inputs originating substantially different outputs. It will be a situation which is undesirable from the control monitoring perspective. Because of continuous structure of output functions, a sugeno FIS is also better and adequate for functional analysis than a mamdani FIS. Figure 2.8 shows the surface view of the fuzzy logic system in case of mamdani inference system. It is very helpful in case of two or more inputs and one output [16].

#### 2.3.6 Defuzzification

Defuzzification converts the fuzzy outputs back to crisp values. There are different defuzzification methods given as:

- Max embership
- Centroid
- Bisector
- Weighted average
- Mean-max
- Center of sum



Figure 2.8: Surface view in the case of a mamdani fuzzy inference system

#### 2.3.7 Control scheme

This section describes the classical control scheme and fuzzy control scheme. In classical control scheme we have open loop and closed loop control architecture. Figure 2.9 shows the classical feedback control structure of a plant. In fuzzy control scheme the conventional controller is replaced by fuzzy logic controller. The fuzzy control scheme is shown in Figure 2.10



Figure 2.9: Classical feedback control scheme



Figure 2.10: Fuzzy logic control scheme 22

The majority of fuzzy logic control systems are knowledge-based systems in that either their fuzzy models or their fuzzy logic controllers are described by fuzzy IF-THEN rules, which have to be established based on experts' knowledge about the systems, controllers, performance, etc. Moreover, the introduction of input-output intervals and membership functions is more or less subjective, depending on the designer's experience and the available information. However, we emphasize once again that after the determination of the fuzzy sets, all mathematics to follow are rigorous. Also, the purpose of designing and applying fuzzy logic control systems is, above all, to tackle those vague, ill-described, and complex plants and processes that can hardly be handled by classical systems theory, classical control techniques, and classical two-valued logic. This is the first type of fuzzy logic control system: the fuzzy logic controller directly performs the control actions and thus completely replaces a conventional control algorithm. Yet, there is another type of fuzzy logic control system: the fuzzy logic controller is involved in a conventional control system and thus becomes part of the mixed control algorithm, so far as to enhance or improve the performance of the overall control system.

The fuzzy logic controller provides an algorithm, which converts the expert knowledge into an automatic control strategy. Fuzzy logic is capable of handling approximate information in a systematic way and therefore it is suited for controlling nonlinear systems and is used for modelling complex systems, where an inexact model exists or systems where ambiguity or vagueness is common. The fuzzy control systems are rule based systems in which a set of fuzzy rules represent a control decision mechanism for adjusting the effects of certain system stimuli. With an effective rule base, the fuzzy control systems can replace a skilled human operator. The rule base reflects the human expert knowledge, expressed as linguistic variables, while the membership functions represent expert interpretation of those variables.

Designing a good fuzzy rule base is the key to obtain satisfactory control performance for a particular operation. Classical analysis and control strategy are incorporated in the rule base. The control literature has worked towards reducing the size of the rule base and optimizing the rule base using different optimization techniques like Genetic Algorithm (GA) and Particle Swarm Optimization (PSO) for

intelligent controller. At last defuzzified output is obtained from the fuzzy inputs [16].

#### 2.3.8 Fuzzy applications

In the decade after Dr. Zadeh's seminal paper on fuzzy sets many theoretical developments in fuzzy logic took place in the United States, Europe, and Japan. From the mid-seventies to the present, however, Japanese researchers have been a primary force in advancing the practical implementation of the theory; they have done an excellent job of commercializing this technology. Fuzzy logic affects many disciplines. In videography, for instance, Fisher, Sanyo, and others make fuzzy logic camcorders, which offer fuzzy focusing and image stabilization. Mitsubishi manufactures a fuzzy air conditioner that controls temperature changes according to human comfort indexes. Matsushita builds a fuzzy washing machine that combines smart sensors with fuzzy logic. The sensors detect the color and kind of clothes present and the quantity of grit, and a fuzzy microprocessor selects the most appropriate combination from 600 available combinations for water temperature, detergent amount and washes and spins cycle times. The Japanese city of Sendai has a 16-station subway system that is controlled by a fuzzy computer. The ride is so smooth that the riders do not need to hold straps, and the controller makes 70 percent fewer judgmental errors in acceleration and braking than human operators do. Nissan introduced a fuzzy automatic transmission and a fuzzy anti-skid braking system in one of their recent luxury cars. Tokyo's stock market has stock-trading portfolios based on fuzzy logic that outperformed the Nikkei exchange average. In Japan, there are fuzzy golf diagnostic systems, fuzzy toasters, fuzzy rice cookers, fuzzy vacuum cleaners, and many other industrial fuzzy control processes.

With increasing complexities in system engineering, the focus of fuzzy control is moving from elementary control problems to higher levels in the system hierarchy such as supervisory control, monitoring and diagnosis, and logistic support. It is to be noted that telecommunications, which is one of the major future industries, has started investigating fuzzy control for communication systems and that several pilot projects have been initiated for tackling routing and overload handling problems. So far, the majority of existing applications are purely software-based. However, general purpose fuzzy logic processors or coprocessors will be found to be useful in extremely time critical applications like pattern recognition task in a complex plant automation and in mass produced automotive electronics. The first generation of fuzzy control in the existing applications exploits only a very small fragment of fuzzy logic theory. In many cases of more complex, ill-structured problems, this first generation technology is not sufficiently equipped to represent and implement the knowledge needed for powerful solutions. Besides, there is strong need for a more systematic design and analysis methodology for fuzzy control applications, spanning the whole life-cycle from perception to all the way up to deployment and maintenance. It must provide answers to make a proper choice of alternative design issues after a thorough analysis of the problem, and must be able to associate variations of parameters to system-performance. At this stage, one should not expect a universal design and optimization strategy for fuzzy control, which will be of some practical use. Such a universal theory does not exist for conventional control engineering either. Instead, we have to proceed from the few isolated islands where we already know exactly how to design a fuzzy control algorithm to clusters of problems and related design methodologies. From the above discussions it is apparent that fuzzy control has tremendous scope in the knowledge based systems approach to closed loop control system, which may be defined as:

A knowledge based system for closed loop control is a system which enhances the performance, reliability and robustness of control by incorporating knowledge which cannot be captured in the analytical model used for controller design and that is taken care of by manual modes of operation or by other safety and ancillary logic mechanism [17].

# **CHAPTER THREE**

# SYSTEM MODELING AND CONTROL DESIGN

# CHAPTER THREE SYSTEM MODELING AND CONTROL DESIGN

# **3.1 Mathematical Modeling**

A mathematical model is developed to describe the dynamics of the boiler drum of a natural circulation boiler. A boiler drum is divided into two parts; the upper part contains saturated steam while the lower part contains a steam/water mixture. Balance equations are applied to the drum. The resulting equations are used to model the drum-level. The importance of the resulting model comes from the direct modeling of boiler which is usually computed off-line with the aid of empirical formulas and assumptions.

The development of a mathematical model for drum type boilers requires a combination of non-linear equations, modeling water level is a quite complicated task because of the complex flow patterns inside the drum. Although the drum level is very important parameter to control for safe operation of boilers, none of the available literature presents a complete model for the system including the drum level [18].

## **3.1.1 Model formulation**

Figure 3.1 shows a schematic diagram of natural circulation drum type boiler. The heat released from the combustion of fuel is used to evaporate water in the riser tubes. The resulting difference in water densities causes the circulating flow of water. Accordingly, the water-steam mixture enters the lower part of the drum. Steam flows out at the top of the drum as demanded. Feed-water makeup is supplied to the lower part of the drum. Modeling of the boiler includes the essential inputs and outputs needed for the overall plant operation and control. In the system the variable, fuel flow, feedwater flow, two actuator flows and the control valve position were considered as input. The recorded outputs were drum pressure, generated electric power, drum level and pressure in various parts of the system [19].



Figure 3.1: The boiler drum

The basic equations used from the Astrom and Eklund work are:

$$\frac{\mathrm{dP}}{\mathrm{dt}} = -0.0018u_2 P^{9/8} + 0.02u_1 - 4.4 \times 10^{-4}u_3$$
(3.1)

$$P_0 = 0.6u_2 p^{9/8}$$
(3.2)

Where  $u_1$  and  $u_3$  are the fuel and feedwater flows in T/hr respectively.  $u_2$  is the control valve position. P and P<sub>0</sub> are the output variables of drum pressure and electrical output. This work was extended by Bell and Astrom (1979) and resulted in the following model:

$$\frac{\mathrm{dP}}{\mathrm{dt}} = -0.0018u_2 P^{9/8} + 0.9u_1 - 0.15u_3 \tag{3.3}$$

$$\frac{\mathrm{d}P_0}{\mathrm{d}t} = \left\{ (0.73u_2 + 0.16)P^{9/8} - P_0 \right\} / 10 \tag{3.4}$$

Where  $u_1$  and  $u_3$  are the fuel and feedwater actuator positions.  $u_2$  is the control valve position. P and P<sub>0</sub> are the drum pressure and electrical output. Note that the differences between the model in Equations. (3.3) and (3.4), and that in (3.1) and (3.2) are:

- The fuel and feedwater flows have been changed to actuator positions, so that all controls are of the same type.
- A differential equation has been used instead of the algebraic equation for the electrical output. This is to include the time lag associated with the steam capacity and inertia of the turbine and alternator.

• An extra constant (0.16) has been included in Equation. (3.4) to allow for the heat energy passing to the condensers and feedheaters.

A further extension by Bell and Astrom (1979) included equations for predicting drum water level. This model had two forms, the simplest being:

$$\frac{\mathrm{dP}}{\mathrm{dt}} = -0.0018u_2 P^{9/8} + 0.9u_1 - 0.15u_3 \tag{3.5}$$

$$\frac{\mathrm{d}P_0}{\mathrm{d}t} = \left\{ (0.73u_2 + 0.16)P^{9/8} - P_0 \right\} / 10 \tag{3.6}$$

$$w_s = (1.1u_2 - 0.19)P \tag{3.7}$$

$$\frac{d\rho_f}{dt} = \frac{141u_3 - w_s}{V_t}$$
(3.8)

$$\rho_{\rm s} = C_{\rm s1} P + C_{\rm s2} \tag{3.9}$$

$$\alpha_{\rm cs} = \frac{1/\rho_{\rm f} - V_{\rm w}}{1/\rho_{\rm s} - V_{\rm w}}$$
(3.10)

$$X_{w} = 50(V_{w}V_{t}\rho + 60\alpha_{cs} + 0.05w_{s} + 65.5)$$
(3.11)

Where  $X_w$  is the output drum water level.  $w_s$ ,  $\rho_f$ ,  $\rho_s$  and  $\alpha_{cs}$  are the intermediate variables steam flow, density of fluid in system, density of steam and quality of steam respectively.  $V_t$ ,  $C_{s1}$ ,  $C_{s2}$  and  $V_w$  are constant representing total volume of the drum and risers, least squares fitting of steam table and specific volume of water. The boiler turbine unit used to evaluate the models in this report is a 160 Mw oil fired natural circulation drum unit. Full details of the unit are shown in Table 3.1 [19].

#### **3.1.2** The linear model

For simplicity the intended stability analysis shall be performed by linearization of the nonlinear model at typical operating points of the drum, a linearized model is obtained

from a truncated Taylor series expansion of the non-linear equations. The non-linear dynamics are of the form:

Parameters	Values
Rated power, P <sub>0</sub>	160MW
Steam flow at rated load, q <sub>s</sub>	140kg/sec
Drum steam pressure, P	$140 \text{kg/} \text{cm}^2$
Superheated steam temperature, T <sub>s</sub>	535°C
Volume of drum, V <sub>d</sub>	$40m^{3}$
Volume of downcomers, V <sub>dc</sub>	11 <i>m</i> <sup>3</sup>
Volume of risers, V <sub>r</sub>	$34m^{3}$
Mass of water in system at normal operating conditions,	40,000kg
M <sub>fw</sub>	
Mass of steam in system at normal operating conditions, $M_s$	2,000kg
Feedwater temperature, T <sub>fw</sub>	300°C
Specific volume of water at 320 °C, Vw	$0.001538m^3$
Constant from fitting data to steam tables, $C_{s1}$	0.8
Constant from fitting data to steam tables, $C_{s2}$	-25.6

Table 3.1: Parameters of boiler turbine 160 Mw in Malmo, Sweden

$$\frac{\mathrm{dx}}{\mathrm{dt}} = \mathrm{f}(\mathrm{x},\mathrm{u}) \tag{3.12}$$

$$y = g(x, u) \tag{3.13}$$

And linearization of the system about the nominal operating point,  $(x^0, u^0)$ , reqires calculating the liner system matrices as follows [2]:

$$A = \left[\frac{\partial f}{\partial x}\right]_{(x^0, u^0)}$$
(3.14)

$$B = \left[\frac{\partial f}{\partial u}\right]_{(x^0, u^0)}$$
(3.15)

$$C = \left[\frac{\partial g}{\partial x}\right]_{(x^0, u^0)}$$
(3.16)

$$D = \left[\frac{\partial g}{\partial u}\right]_{(x^0, u^0)}$$
(3.17)

For  $x^0 = [108 \ 74.65 \ 428]^T$  and  $u^0 = [0.34 \ 0.69 \ 0.436]^T$ . The linear approximation to the system is:

$$\frac{d\bar{x}}{dt} = A\bar{x} + B\bar{u}$$
(3.18)  
$$\bar{y} = C\bar{x} + D\bar{u}$$
(3.19)

Where  $\bar{x}=x-x^0$  ,  $\bar{y}=y-y^0$  , and  $\bar{u}=u-u^0.$  The linear system matrices are found to be:

$$A = \begin{bmatrix} -2.509 \times 10^{-3} & 0 & 0\\ 6.94 \times 10^{-2} & -0.1 & 0\\ -6.69 \times 10^{-3} & 0 & 0 \end{bmatrix}$$
$$B = \begin{bmatrix} 0.9 & -0.349 & -0.15\\ 0 & 14.155 & 0\\ 0 & -1.389 & 1.659 \end{bmatrix}$$
$$C = \begin{bmatrix} 1 & 0 & 0\\ 0 & 1 & 0\\ 6.34 \times 10^{-3} & 0 & 4.71 \times 10^{-3} \end{bmatrix}$$
$$D = \begin{bmatrix} 0 & 0 & 0\\ 0 & 0 & 0\\ 0.253 & 0.512 & -0.014 \end{bmatrix}$$

Figure 3.2 below shown the state space model and how to input it's parameters in MATLAB/SIMULINK.

#### **3.2 Actuator Dynamics**

If control studies are to be under taken with the models presented in this work, then actuator dynamics will be needed. The actuator dealing with the positioning is modeled as a 1st order lag element whose integrator saturation corresponds to the valve position ranging between 0% and 100%. Figure 3.3 gives a block diagram for the realization of such dynamics [17]



Figure 3.2: State space model



Figure 3.3: Representation of actuator dynamics

#### 3.2.1 Fuel flow

The rate limiting for the actuator used to operate the fuel flow valve is by the equation:

$$\left|\frac{du_1}{dt}\right| \le \frac{0.007}{second} \qquad \qquad 0 < u_1 < 1 \tag{3.20}$$

Figure 3.4 shows the simulation of fuel flow actuator and setting limit rate in MATLAB.

	Rate Limiter Limit rising and falling rates of signal.	
Integrator Limited1	Parameters Rising slew rate:	
	- 0.007 Falling slew rate:	
	-0.007	
Integrator Limited2	Sample time mode: continuous           Image: Treat as gain when linearizing	•
	OK Cancel Help App	ply

Figure 3.4: Fuel actuator

### 3.2.2 Feedwater flow

The rate limiting for the actuator used to operate the feedwater flow valve is by the equation:

$$\left|\frac{du_3}{dt}\right| \le \frac{0.05}{second} \qquad \qquad 0 < u_3 < 1 \tag{3.21}$$

Figure 3.5 shows the simulation of feedwater flow actuator and setting limit rate in MATLAB.

## **3.2.3** Control valve

The rate limiting of opening and closing for the actuator used to the power output valve is by the equation:

## i. Opening or upper rate

$$\left|\frac{du_2}{dt}\right| \le \frac{0.2}{second} \tag{3.22}$$

ii. Closing or lower rate limit

$$\left|\frac{du_2}{dt}\right| \le \frac{2}{second} \tag{3.23}$$

 $0 < u_1 < 1$ 

Figure 3.6 shows the simulation of control valve actuator and setting for upper rate and lower rate limit in MATLAB.

Limited1   Imited1   Integrator   Limited3   Rate Limite Parameters Rising slew rate: Integrator Limited2 Rate Limite Rate Limite Parameters Rising slew rate: 0.05 Falling slew rate: -0.05 Sample time mode: continuous Treat as gain when linearizing	Integrator	Rate Limite 🔁 Fun	nction Block Parameters: Rate Limiter2
<ul> <li>Limit rising and falling rates of signal.</li> <li>Parameters</li> <li>Rising slew rate:</li> <li>Integrator</li> <li>Integrator</li> <li>Rate Limite</li> <li>Rate Limite</li> <li>Rate Limite</li> <li>Rate Limite</li> <li>Co5</li> <li>Falling slew rate:</li> <li>-0.05</li> <li>Sample time mode: continuous</li> <li>Treat as gain when linearizing</li> </ul>	Limited1	Rate	Limiter
S       J       Parameters         Integrator       Rate Limite       Parameters         Integrator       Integrator       Rate Limite         Integrator       Rate Limite       Parameters         Integrator       Rate Limite       Parameters         Integrator       Rate Limite       Parameters         Sample time mode:       continuous       Integrator         Integrator       Treat as gain when linearizing       Integrator		Limit	rising and falling rates of signal.
Limited3       Rising slew rate:         1       Integrator         Limited2       Rate Limite         Rate Limite       -0.05         Sample time mode:       continuous         Image: Treat as gain when linearizing	Integrator	Rate Limite Para	meters
1       1       0.05         Integrator       Rate Limite       -0.05         Sample time mode:       continuous       •         Image: Continuous       •	Limited3	Risin	ng slew rate:
Integrator       Rate Limite       Falling slew rate:         Limited2       -0.05         Sample time mode:       continuous         Image: Ima			5
Limited2 -0.05 Sample time mode: continuous ▼ ✓ Treat as gain when linearizing	Integrator	Rate Limite Fallin	ng slew rate:
Sample time mode: continuous	Limited2	-0.0	)5
Treat as gain when linearizing		Sam	ple time mode: continuous
		IT 🔍	reat as gain when linearizing
			OK Cancel Help Apply

Figure 3.5: Feedwater actuator

	Function Block Parameters: Rate Limiter3	23
	Rate Limiter	
	Limit rising and falling rates of signal.	
Integrator Rate Limit	Parameters	
Limited1	Rising slew rate:	
	0.02	
Integrator Rate Limit	Falling slew rate:	
Limited3	-2	
	Sample time mode: continuous	•
Integrator Limited2	Treat as gain when linearizing	
	OK Cancel Help	Apply

Figure 3.6: Control valve

# **3.3 System Control Design**

In this section, typical methods used to develop a conventional PI controller and Fuzzy Logic Controller (FLC) by using MATLAB/SIMULINK. The target of the thesis is

control the boiler for the pressure, power output and water level. The result for both controller simulations are compared and discuss in chapter four.

#### 3.3.1 PI controller design

Some applications may require using only one or two modes to provide the appropriate system control. This is achieved by setting the gain of undesired control output to zero. A PID controller will be called a PI, PD, P or I controller in the absence of the respective control action. PI controllers are particularly common, since derivative action is very sensitive to measurement noise, and the absence of an integral value may prevent the system from reaching its target value due to the control action. Now investigate the design of PI controller to control the boiler. To controls the pressure and water level of the drum to coincide with desired pressure and water level by changing fuel flow valve ratio and feedwater flow valve ratio.

Figure 3.7 shows the Simulink block diagram of PI controller. Simulink continuous PID block offers functionalities which meets exactly our needs, it can easy configuration by set controller parameter as shown in Figure 3.7. A separate PI controller has been designed for any variable (pressure, water level and power output) without considering any sort of coupling or interaction between both outputs. In the coupled PI controller design the gains are tuned in two stages. The first stage consists of tuning the proportional gains in the PI controller only and leaving the others fixed at zero. The initial gains are selected at random between some coarse upper and lower bounds and tuned through iteration. Once some pre-specified convergence criterion has been achieved, the best fit triplet of proportional gains is designated as the result for the stage. The second stage is to tuning the integral gain of the three control units. In the same way, the selection of gain begins randomly and through repetition until the required response are met. The results of tuning PI controller in Table 3.2.



Figure 3.7: The SIMULINK block diagram of PI controller

Table 3.2	: PI controller	parameters

PI-Controller Parameters			
Controller	k <sub>p</sub>	k <sub>I</sub>	
Pressure	3	0.001	
Power output	0.3	0.0001	
Water level	40	0.001	

## 3.3.2 Fuzzy controller design

The most important aspect in fuzzy logic control system designs start with a process of converting the measured inputs called crisp values, into the fuzzy linguistic values used by the fuzzy reasoning mechanism. The process of reasoning mechanism will perform fuzzy logic operations and result the action according to the fuzzy inputs. A collection of the expert control rules known as knowledge needed to achieve the control goal.

In this fuzzy model there are three controller (pressure, power output and water level), for the two input variable of fuzzy system the Error (E) and Change in Error (CE). And the fuel flow valve position, steam control valve position and feedwater

flow valve position are outputs corresponding to the pressure, power output and water level respectively.

#### 3.3.3 Fuzzy logic toolbox

There are five primary Graphical User Interface (GUI) tools for building, editing and observing fuzzy inference systems in the toolbox. These GUI are dynamically linked and if the changes make to the FIS to one of the toolbox, the effect can be seen in other GUIs:

#### A. Fuzzy inference system editor

The FIS editor displays information about a fuzzy inference system. To open the fuzzy logic designer, type Fuzzy command at the MATLAB on command window appears as shown in Figure 3.8. The FIS editor opens and displays a diagram of the fuzzy inference system with the names of each input variable on the left, and those of each output variable on the right, as shown in the Figure 3.8. The sample membership functions shown in the boxes are just icons and do not depict the actual shapes of the membership functions. Note: in this work, two FIS files are designed, one for pressure and power output other one for drum water level.



Figure 3.8: Pressure and power output FIS

#### B. Membership function editor

The membership function editor tool is used to display and edit all of the membership functions associated with all of the input and output variables for the entire fuzzy inference system. The membership function editor shares some features with the FIS editor. A triangular membership functions are used for the fuzzy set of input and output vectors. Different linguistic variables are considered and details of these variables are shown in Table 3.3.

	Error (E) Change		Change in Error (CE)		ntroller Output (U)
NL	Negative Large	NL	Negative Large	FC	Fully Close
NM	Negative Medium	NM	Negative Medium	С	Close
Ζ	Zero	Ζ	Zero	М	Medium
PM	Positive Medium	PM	Positive Medium	0	Open
PL	Positive Large	PL	Positive Large	FO	Fully Open

Table 3.3: Linguistic variables of fuzzy set

Triangular membership functions for pressure and power output, Figure 3.9 shows the membership function of the input error (E), Figure 3.10 shows the membership function of the input change in error (CE) and Figure 3.11 shows the membership function of the output valve position. The second fuzzy set designed for water level, Figure 3.12 shows the membership function of the input error (E), Figure 3.13 shows the membership function of the input change in error (CE) and Figure 3.14 shows the membership function of the output valve position.



Figure 3.9: Input 1 (Error) in FIS editor for pressure and power



Figure 3.10: Input 2 (DError) in FIS editor for pressure and power



Figure 3.11: Output (Valve position) in FIS editor for pressure and power



Figure 3.12: Input 1 (Error) in FIS editor for level



Figure 3.13: Input 1 (DError) in FIS editor for level



Figure 3.14: Output (Valve position) in FIS editor for level

#### C. Rule editor

Constructing rules using the graphical rule editor interface is fairly self-evident. Based on the descriptions of the input and output variables defined with the FIS editor, the rule editor allows to construct the rule statements automatically. As shown in Figure 3.15 with rule editor it can:

- Create rules by selecting an item in each input and output variable box, selecting one connection item, and clicking add rule. It can choose none as one of the variable qualities to exclude that variable from a given rule and choose not under any variable name to negate the associated quality.
- Delete a rule by selecting the rule and clicking delete rule.
- Edit a rule by changing the selection in the variable box and clicking change rule.
- Specify weight to a rule by typing in a desired number between 0 and 1 in weight. If you do not specify the weight, it is assumed to be unity (1).

Rule Editor: Pres	sure&Power	
le Edit View	Options	
2. If (Error is Z) ar 3. If (Error is Z) ar 4. If (Error is Z) ar 5. If (Error is Z) ar 5. If (Error is PM) 7. If (Error is PM) 8. If (Error is PM) 9. If (Error is PM) 10. If (Error is PL) ar 12. If (Error is PL) ar 13. If (Error is PL) ar 14. If (Error is PL) ar 15. If (Error is PL)	ad (DError is NM) then (ValvePosition is C) (1) d (DError is Z) then (ValvePosition is M) (1) id (DError is PM) then (ValvePosition is O) (1) and (DError is NL) then (ValvePosition is O) (1) and (DError is NL) then (ValvePosition is M) (1) and (DError is NL) then (ValvePosition is M) (1) and (DError is Z) then (ValvePosition is O) (1) and (DError is PL) then (ValvePosition is O) (1) and (DError is PL) then (ValvePosition is FO) (1) and (DError is NL) then (ValvePosition is FO) (1) and (DError is NL) then (ValvePosition is M) (1) and (DError is NL) then (ValvePosition is M) (1) and (DError is NL) then (ValvePosition is O) (1) and (DError is Z) then (ValvePosition is O) (1) and (DError is Z) then (ValvePosition is O) (1) and (DError is Z) then (ValvePosition is Z) (1) and (DError is PM) then (ValvePosition is S) (1) and (DError is PM) then (ValvePosition is S) (1) and (DError is Z) then (ValvePosition is Z) (1) and (Z)	E
f Error is NL A	and DError is       NL       NM       Z       PM       PL       none	Then ValvePosition is FC C M O FO none
Onot	🗖 not Weight:	inot.
<ul><li>or</li><li>and</li></ul>	1 Delete rule Add rule Change rule	e << >>
IS Name: Pressure	&Power	Help Close

Figure 3.15: Rule editor

Table 3.4 shows the corresponding rule table for the proposed fuzzy control system. The top row of the matrix indicates the fuzzy sets of the error variable E and the left column indicates the change in error variable CE and the output variable U is shown in the body of the matrix.

CEE	NL	NM	Z	PM	PL
NL	FC	FC	С	С	М
NM	FC	С	С	М	0
Z	С	С	М	0	0
PM	С	М	0	0	FO
PL	М	0	0	FO	FO

Table 3.4: Rule base for fuzzy logic controller

#### D. The rule viewer

Figure 3.16 shows the rule viewer, it is allows to interpret the entire fuzzy inference process at once. The rule viewer also shows how the shape of certain membership functions influences the overall result. Because it plots every part of every rule, it can become unwieldy for particularly large systems, but, for a relatively small number of inputs and outputs, it performs well (depending on how much screen space you devote to it) with up to 30 rules and as many as 6 or 7 variables.

#### E. The surface viewer

Upon opening the surface viewer, a three-dimensional curve are seen that represents the mapping from food and service quality to tip amount. Because this curve represents a two-input one-output case, it can see the entire mapping in one plot. When moves beyond three dimensions overall, to encounter trouble displaying the results are started. The surface viewer has a special capability that is very helpful in cases with two (or more) inputs and one output: the axes can be grabbed, using the mouse and reposition them to get a different three-dimensional view on the data as shown in Figure 3.17.



Figure 3.16: The rule viewer



Figure 3.17: The surface viewer

# CHAPTER FOUR SYSTEM SIMULATION RESULTS AND DISCUSSIONS

## **CHAPTER FOUR**

# SYSTEM SIMULATION RESULTS AND DISCUSSIONS

## **4.1 Introduction**

Computer modeling and simulation is widely used to study the behavior of proposed system and to decide whether the new control design processes are valid in order to avoid the mistakes early in simulations before actual real implementation. As has been stated before, the controller cannot be tested on a real boiler system. To simulate the system, a MATLAB/SIMULINK is used. This chapter show the simulation results of the uncontrolled boiler turbine, also shows the simulation results of the PI controller and the fuzzy logic controller. The duration of the simulation is 1000 seconds, which is enough to view the response of the component and overall system. And setpoint values are choice as below:

 $Pressure = 108 kg/cm^2$ 

Power output = 74.65 MW

Water level = 0m

#### 4.2 Uncontrolled System

The close loop response was studied by simulating the model consisting of the boiler turbine unit and actuator valves with feedback control system. This response gives a good initial indication of a model potential.

Figure 4.1 is the Simulink model for the boiler without any controller. It also shows the pressure output used as feedback for fuel flow rate, power output used as feedback for steam control and the water level used as feedback for feedwater flow rate. The feedback system compare the set point with actual output then produce the error signal. The actuator receive error signal and work to limit it between 0 and 1, the valve open or close according to this value. This process continues to seek access to the reference value.



Figure 4.1: Simulink model of uncontrolled boiler turbine

Figure 4.2 shows the response of the pressure. Figure 4.3 shows the response of the power output also oscillating. Figure 4.4 shows the response of the water level.



Figure 4.2: Pressure response for uncontrolled system



Figure 4.3: Power output response for uncontrolled system



Figure 4.4: Water level response for uncontrolled system

#### 4.3 System with PI Controller

In this section want to know how to controls boiler turbine using conventional PI controller. As mentioned earlier in chapter two, PI control is a popular conventional approach. The parameter calculated in previous chapter (Table 3.3). The simulation and results of PI controller as below. This scheme in conventional method to control boiler turbine a separate PI controller are used for any output variables with feedback system as shown in Figure 4.5. A PI controller attempts to correct the error between

a measured process variable and a desired set point by calculating and then outputting corrective action that can adjust the process accordingly and rapidly, to keep the error minimal.



Figure 4.5: Simulink model of boiler turbine using PI controller

Figure 4.6 shows the pressure response with PI controller it can observe that the response of the pressure still oscillating with little steady state error but there is big overshoot. Figure 4.7 shows the power output response with PI controller, overshoot is illustrated. Figure 4.8 shows water level response with PI controller initially increases due to feedwater. After that decrease unit pressure stabilizes then oscillating.



Figure 4.6: Pressure response with PI controller



Figure 4.7: Power output response with PI controller



Figure 4.8: Water level response with PI controller

#### 4.4 System with Fuzzy Logic Controller

The objective of this study is to develop a control system for the boiler using a fuzzy logic controller. The Simulink block diagram and results are shown below In Figure 4.9 shows the Simulink model of boiler turbine using fuzzy controller it's seen that there is individual fuzzy controller for each variable with feedback from output to compare with the set point and then produce the error. Fuzzy controller has two input error and change in error. First input the error is taken directly from the comparison and change in error through derivative function. A gains for inputs error and change in error are used to scale the signal to be suitable with membership function.



Figure 4.9: Simulink model of boiler turbine using fuzzy logic controller

In this study. The performance of the drum pressure, power output and level for fuzzy logic controller instead conventional controller is illustrated. Figure 4.10 shows the pressure response with fuzzy controller. It started increasing slowly until it reaches the set point. Also we observed there is no overshoot. In Figure 4.11 shows the power output response with fuzzy controller, it increasing depend on the pressure. After the pressure reaches enough value it will settle down. Figure 4.12 shows the water level response. The drop pressure in the start across the feedwater causing increasing in water level. Oscillation in the water level is a results of the steam mass fraction and steam bubbles under the water.



Figure 4.10: Pressure response with fuzzy controller



Figure 4.11: Power output response with fuzzy controller



Figure 4.12: Water level response with fuzzy controller

#### 4.5 Comparison and Discussions

In order to validate the control system strategies as described in this study digital simulation were carried out on a converter boiler turbine whose model are given in chapter three. The results of the system under study with PI controller and fuzzy controller are compared with reference. Figure 4.13 shows the compare pressure response, Figure 4.14 shows the compare power output response, and Figure 4.15 shows the compare water level response.



Figure 4.13: Pressure response with PI controller and fuzzy controller



Figure 4.14: Power output response with PI controller and fuzzy controller



Figure 4.15: Water level response with PI controller and fuzzy controller

First a comparison has been made for drum pressure in terms of rising time, settling time and maximum overshoot between three types of control illustrated in Table 4.1.

Type of	Rising Time	Settling	
Control	(10%-90%)	Time	Overshoot
	(sec)	(sec)	(%)
Uncontrolled	144.6	720.17	27.56
PI Controller	143.8	541.41	24.37
Fuzzy Controller	306.77	394.39	-

Table 4.1: Pressure response comparison

Second a comparison has been made for power output in terms of rising time, settling time and maximum overshoot between three types of control illustrated in Table 4.2.

Type of Control	Rising Time (10%-90%)	Settling Time	Overshoot
	(sec)	(sec)	(%)
Uncontrolled	126.31	730.3	24.41
PI Controller	124.85	551.75	28.6
Fuzzy Controller	231.33	295.71	-

 Table 4.2: Power output response comparison

Third a comparison has been made for water level between the maximum values and the error. The results shown in Table 4.3.

Type of	Maximu		
Control	Value	Time	Error
	(m)	(sec)	(m)
Uncontrolled	0.6008	191	0.498
PI Controller	0.6041	197.21	0.0491
Fuzzy Controller	0.3377	150.6	0.0120

Table 4.3 Water level response comparison

The performance of the system with controllers has been designed are illustrated in figures and tables above contains the controller responses of each one. For both no controller and PI controller the drum pressure is very oscillatory with a large overshoot (27.56%, 24.41) respectively. The response settles out with a steady state error of (4.38, 2.8)kg/ $cm^2$  for no controller and PI respectively. The drum pressure using fuzzy controller achieved good response there is no oscillating and overshoot with settling time 377.6sec and steady state error 0.33kg/ $cm^2$ .

The power output responses are not good for system in cases PI controller and no controller. But for fuzzy controller the results is good there is no overshoot and achieved settling time 383.72 sec and steady state error 0.14MW. The water level response has high maximum values for no controller and PI controller (0.6m) that can causing shutdown of the boiler. Furthermore in case no controller the error is big. The result of fuzzy controller is acceptable.

# **CHAPTER FIVE**

# **CONCLUSION AND RECOMMANDATIONS**

# CHAPTER FIVE CONCLUSION AND RECOMMANDATIONS

# **6.1 Conclusion**

In this study a fuzzy logic based controller for boiler turbine has been studied. First of all a mathematical model of the system was developed and a conventional PI controller was implemented. The PI controller gave a very high overshoot and high settling time. So an artificial intelligence technique has been proposed and developed. A fuzzy logic controller has been implemented. The results was compared with the conventional controller response. The design of the fuzzy logic controller has been explained and the performance was evaluated. The simulation results indicate that FLC provides the best performance with compared with PI controller, and the shape of the FLC surface is smoother than that of PI controller. In Fuzzy logic control it is not necessary to change the control parameters at any conditions. It is clear that the fuzzy controller is more advantageous than conventional PI because the settling time is short compared with the conventional PI controller. Fuzzy controller gives better dynamic response. This proposed scheme is very suitable for applications of industrial position control drives.

# **6.2 Recommendations**

- To make the control system more efficient, a model of the complete processes with other variables like temperature and air flow rate is needed.
- Apply the system in real time.
- Use of neural networks and genetic algorithm for adjusting fuzzy rules and selecting inputs and outputs membership functions.
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