

بسم الله الرحمن الرحيم

: قال تعالى

قَالَ الَّذِي عِنْدَهُ عِلْمٌ مِّنَ الْكِتَابِ أَنَّا إِلَيْكَ
بِهِ، قَبْلَ أَنْ يَرْتَدَ إِلَيْكَ طَرْفُكَ فَلَمَّا رَأَهُ مُسْتَقِرًا عِنْدَهُ، قَالَ هَذَا
مِنْ فَضْلِ رَبِّي لِي بِلُوْنِي، أَشْكُرُ أَنْ كُفُورًا وَمَنْ شَكَرَ فَإِنَّمَا يُشْكُرُ
لِنَفْسِهِ، وَمَنْ كَفَرَ فَإِنَّ رَبِّي عَنِّي كَرِيمٌ ﴿٤٠﴾

صدق الله العظيم
(سورة النمل آية 40)

DEDICATION

Dedicated to:

My mother

My father

My wife

My family and my friends

My colleagues in Garri 4 Power Plant

With my love and respect

ACKNOWLEDGMENT

Thanks **God** in the first

Thanks to my supervisor

Prof. Sabir Mohammed Salih

For his assistance, guidance and endless help throughout the steps of this research work.

Thanks for any one helped me to make this work

Asim Abd Alla Salih

ABSTRACT

Garri4 Steam Power Plant works with regeneration Rankine cycle, It consists of two steam turbines each one generates 55 MW. In the Rankine cycle the steam jet air ejector or vacuum pump are utilized to generate and preserve vacuum in the condenser. Steam jet air ejector is simpler, lower cost, more reliable than vacuum pump , and does not consists of moving parts that need to be adjusted or repaired. Steam jet air ejector was installed in Garri4 but in commissioning operation ejector failed and did not satisfy the vacuum requirement for proper operation. To solve this problem two solutions were suggested and worked out, the first one is to replace the condensate water by fresh cooling water in the ejector's cooler, but also it still failed and the

second is to replace air ejector by vacuum pump which made vacuum sufficient to run the plant at full load.

In this thesis, the problem of the air ejector had been studied; also reasons of its failure, the effect of replacing air ejector by vacuum pump on plant efficiency, selection and the necessary modifications for the pump had been attained. The research method in this thesis is a theoretical survey case study. It was found that the main air ejector failure is due to design calculations errors of the ejector inner cooler, the pump was selected according to the capacity required of (1550. The pump type is two stage, liquid ring vacuum Pump. The replacing steam jet air ejector by vacuum pump allows the plant to run at full load (55MW), with high performance and a considerable efficiency of (25.46%) and a few required modifications. It is observed that the vacuum pump's running and maintenance cost are higher than ejector's that consumes (55 kWh) more than ejector's (36.86 kWh).The pump works permanently so, the power loss is (18.14 kWh) equivalent to (156.73 MW) per year; then the cost is about (109711 SDG) per year. From these calculations and considerations, it is obvious that recalculation, redesigning and installing of air ejector are convenient enough because of the lower costs. It is recommended to redesign and use the air ejector instead of vacuum pump utilization.

مختصر مس

تعمل محطة قرى 4 البخارية لتوليد الكهرباء بواسطة دورة رانكن، وهى تتكون من وحدتين تنتج كل وحدة 55 ميجاواط. فى دورة ران肯 يعمل قاذف الهواء بواسطة منفذ البخار أو المضخة الخوائية على توليد الخواص والمحافظة عليه داخل المكثف. عند المقارنة بين قاذف الهواء بواسطة منفذ البخار والمضخة الخوائية فإن قاذف الهواء بواسطة منفذ البخار أقل تكلفة، أكثر فاعلية، أبسط ولا توجد به أجزاء متحركة تحتاج إلى صيانة أو إعادة ضبط. تم تركيب قاذف الهواء بواسطة منفذ البخار في محطة قرى 4، لكن في التشغيل التجاري فشل قاذف الهواء في تلبية متطلبات الفراغ (الخواص) في المكثف من أجل تشغيل أمثل للمحطة، تم تقديم وعمل مقترن لحل هذه المشكلة، الاول استبدال المياه المكثفة بمياه التبريد لتبريد المبرد الداخلي لا قاذف لكنه أيضاً فشل، والثانى استبدال قاذف الهواء بالمضخة الخوائية مما صنع خواص كافية لتشغيل المحطة بالطاقة القصوى.

في هذا البحث تمت دراسة مشكلة قاذف الهواء ومحاولة معرفة الأسباب التي أدت لفشلها، وتأثير إستبداله بالمضخة الخوائية على الكفاءة الكلية للمحطة، والتعديلات الضرورية لتركيب المضخة، وكذلك دراسة كيفية اختيار المضخة، وطريقة البحث في هذه الأطروحة هي دراسة نظرية للحالة. وتم التوصل في الدراسة إلى أن سبب فشل قاذف الهواء بواسطة منفذ البخار هو خطأ في تصميم المبرد الداخلي لا قاذف وحساب الحمل التبريدي له، وأن اختيار المضخة تم وفقاً للسعة المطلوبة (1550 م³/س) ونوع المضخة هو حلقة السائل مرحلتين. وأن إستبدال قاذف الهواء بالمضخة الخوائية سمح للمحطة بالعمل بالطاقة القصوى (55 ميغاواط) وأداء عالي وكفاءة (24.46%) وتعديلات مطلوبة طفيفة. ولوحظ ان تكلفة صيانة وتشغيل المضخة أعلى من قاذف الهواء، حيث أن المضخة تستهلك (55 كواتس) وهو أعلى من إستهلاك قاذف الهواء (36.86 كواتس)، ونسبة لعمل المضخة المتواصل فإن نسبة الفاقد في الكهرباء (14.14 كواتس) ما يعادل (156.73 ميغاواط) في السنة وهي تساوى (109711 جنيه) وهي كافية لتكلفة إجراء بحث وإعادة تصميم القاذف من جديد وتركيبه ولذلك تمت التوصية في هذه الدراسة بإعادة تصميم واستخدام القاذف بدلاً من إستخدام المضخة الخوائية.

CONTENTS

الآية القراءية.....	I
Acknowledgment.....	II
Dedication.....	III
Abstract.....	IV
<u>مسنون</u>	V
List of Figures	IX
Abbreviation.....	XI
List of symbols.....	XII

Chapter 1: Introduction.....	1
1.1 Electricity supply in Sudan.....	1
1.1.1 Electrical system in Sudan.....	2
1.1.2 Total installed generation in the national grid.....	2
1.2. Garri-4 power plant.....	2
1.3. The problem definition.....	3
1.4 The problem's Solutions.....	
	4
1.5 About the thesis	4
Chapter 2: Theoretical background.....	6
2.1 Introduction.....	6
2.2 The Ideal Rankine cycle	8
2.3 Methods of Increasing the Efficiency of the Rankine Cycle.....	10
2.3.1. Decreasing the condenser pressure	10
2.3.2. Need of A condenser	11
2.3.3. Direct contact condenser	12
2.3.4. Surface condenser.....	13
2.3.5 Air removal	15
Chapter 3: Steam jet air ejector and vacuum pump.....	17
3.1 Introduction to Vacuum.....	17
3.2 Steam jet air ejector.....	17
3.2.1 Multi-stage ejector sets.....	18
3.2.2 Advantages of steam jet ejectors.....	20
3.3 Vacuum pump.....	23
3.3.1 Vacuum pump types.....	24
3.3.1.1 Liquidring Vacuum Pump	24
3.3.1.2 Principle of Operation.....	24
3.3.1.3 Radial Blower.....	26
3.3.1.4 Rotary Vane.....	26
3.3.2 Factors affecting the performance of vacuum pump.....	27
3.3.2.1 Altitude Effects.....	27
3.3.2.2 Effect of Saturated Air Service on the Capacity of Liquidring Vacuum Pumps.....	28
3.3.2.3 Effect of Service water Temperature on the Capacity of Liquidring Vacuum Pumps.....	29
Chapter 4. Garri (4)power plant.....	32
4.1 Introduction.....	32
4.2. Site location.....	32

4.3. Weather condition.....	33
4.4. Design operating condition.....	33
4.5. Plant configuration.....	33
4.6. Circulating Fluidized Bed (CFB) boiler	35
4.6.1 The advantages of CFB boiler	36
4.6.2 The disadvantage of CFB boiler's technology.....	37
4.7 Sponge coke	38
4.7.1 Sponge coke feeding system	28
4.8 Steam turbine	38
4.8.1 Brief working principle of impulse steam turbine	39
4.8.2 Structure composition of steam turbine	39
4.8.3 Main technical specifications	39
4.8.4 Steam Turbine Systems.....	41
4.8.4.1 Main Steam and High Pressure Bypass System.....	41
4.8.4.2 Main Condensate Systems.....	41
4.9 Condenser.....	42
4.9.1 Condensate Extraction Pump	42
4.9.2 Sponge ball cleaning device.....	42
4.10 Gland Steam Cooler.....	42
4.11 Low Pressure Heaters.....	43
4.12 Deaerator.....	44
4.12.2 Deaerator Components	45
4.13 Feed Water System.....	46
4.13.1 Feed Water Pump.....	46
4.13.2 High and low Pressure Heaters	46
4.14 Bleeding Steam System	47
4.15 Gland Steam Systems.....	48
Chapter 5: Result and Discussion.....	49
5.1 Discussion	49
5.1.1 Main air ejector.....	49
5.1.2 Start air ejector	51
5.2 Problem definition	52
5.3 Replacing condensate water by cooling water.....	53
5.4 Disadvantages of replacing condensate water by cooling water on the ejector cooler.....	54
5.5 Vacuum pump supplier.....	55
5.6 Pump selection.....	55
5.7 Modifications for vacuum pump.....	57
5.8 Replacing air ejector by vacuum pump effects on plant efficiency	58

5.9 Comparison between steam jet air ejector and vacuum pump.....	58
5.9 Results	61
Chapter 6: Conclusion and Recommendation.....	62
6.1 Conclusion	62
6.2 Recommendations.....	63
References	64

List of Figures

Figure		Page NO
<i>Fig. (2.1)</i>	<i>Schematic of a Vapor Power Plant</i>	6
<i>Fig.(2.2)</i>	<i>Schematic of the Rankine Cycle</i>	8
<i>Fig.(2.3)</i>	<i>T-s Diagram of an Ideal Rankine Cycle</i>	10
<i>Fig.(2.4)</i>	<i>The Effect of Lowering the Condenser Pressure</i>	11
<i>Fig. (2.5)</i>	<i>A surface condenser with two passes on the water side</i>	14
<i>Fig.(2.6)</i>	<i>Single pass condenser</i>	15
<i>Fig.(2.7)</i>	<i>Condenser shell pressure and temperature</i>	16
<i>Fig. (3.1)</i>	<i>Steam jet air ejector</i>	18
<i>Fig.(3.2)</i>	<i>Tow stage steam jet air ejector with inter condenser and after condenser</i>	19
<i>Fig.(3.3)</i>	<i>Multi-stage ejector sets</i>	20
<i>Fig.(3.4)</i>	<i>Garri 4 P&ID Drawing of main condensate system</i>	22
<i>Fig.(3.5)</i>	<i>Chief components of a typical mechanical pump, the rotary oil-seal pump</i>	23
<i>Fig.(3.6)</i>	<i>Liquidring vacuum pump</i>	24

<i>Fig.(3.7)</i>	<i>Running of liquid ring vacuum pump</i>	25
<i>Fig.(3.8)</i>	<i>Liquid ring vacuum pump</i>	25
<i>Fig.(3.9)</i>	<i>Radial blower vacuum pump</i>	26
<i>Fig.(3.10)</i>	<i>Rotary Vane vacuum pump</i>	27
<i>Fig. (3.11)</i>	<i>Curves for atmospheric pressure relative to altitudes</i>	28
<i>Fig.(3.12)</i>	<i>Average condensing factors for vacuum pumps in saturated air service</i>	29
<i>Fig.(3.13)</i>	<i>The temperature of the sealing water effect on the capacity</i>	31
<i>Fig. (4.1)</i>	<i>T-S Diagram of an Ideal Regenerative Rankin Cycle with One Open Feed water</i>	32
<i>Fig.(4.2)</i>	<i>Garri4 Power Plant Model</i>	35
<i>Fig.(4.3)</i>	<i>The principle chart of CFB boiler</i>	36
<i>Fig.(4.4)</i>	<i>Coke Feeder</i>	38
<i>Fig.(4.5)</i>	<i>Main Steam and High Pressure Bypass System</i>	41
<i>Fig. (4.6)</i>	<i>Fig. (4.6) Diagram of main condensate system</i>	41
<i>Fig.(4.7)</i>	<i>Low pressure heaters</i>	43
<i>Fig. (4.8)</i>	<i>Deaerator</i>	45
<i>Fig. (4.9)</i>	<i>Fig. (4.9) Diagram of feed water system</i>	46
<i>Fig.(4.10)</i>	<i>High pressure heaters</i>	47
<i>Fig. (5.1)</i>	<i>Garri-4 main air ejector</i>	50
<i>Fig.(5.2)</i>	<i>Garri-4 Start air ejector</i>	53
<i>Fig.(5.3)</i>	<i>cooler of the main air ejector (water side)</i>	53
<i>Fig.(5.4)</i>	<i>replacing condensate water by fresh cooling water on the ejector cooler</i>	54
<i>Fig.(5.5)</i>	<i>Garri-4 liquid ring vacuum Pumps</i>	56
<i>Fig(5.6)</i>	<i>NASH TC/TCM Two Stage, liquid ring vacuum Pumps</i>	56
<i>Fig.(5.7)</i>	<i>Range of capacity of NASH TC/TCM Series vacuum pump</i>	57
<i>Fig. (5.8)</i>	<i>dimensions of the vacuum pump</i>	60

List of symbols

symbols	Meaning	Unit
H	Specific enthalpy of steam	kJ/kg
	amount of work	kJ/kg
	amount of heat	kJ/kg
	saturation pressure	kg/m ²
	saturation temperature	K
	characteristic gas constant	kJ/kg K
W _s	amount of motive steam	kg/h
W _v	Amount of suction vapour	kg/h

Abbreviation

Efficiency

NEC	National Electricity Corporation Sudan
CMEC	China National Machinery and Equipment Import and Export Corporation
SJAE	Steam jet air ejector
CFM	Cubic Feet per Minute
PD	piston displacement
CFB	Circulating Fluidized Bed Boilers
LP	Low Pressure
HP	High pressure
CCW	circulation cooling water
I&C	Instrument and control system
MWh	Mega watt hour